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STANDARDS DEVELOPMENT BRANCH ONDE



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APPENDIX I
CALIBRATION DATA

APPENDIX II
TEST DATA AND CALCULATIONS

APPENDIX III
NATURAL GAS COMPOSITION

ARB-TDA- REPORT NO. 60-80B

17273

Ministry
of the
Environment

The Honourable
Harry C. Parrott, D.D.S.,
Minister

Graham W. S. Scott, Q.C.,
Deputy Minister

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STANDARDS DEVELOPMENT BRANCH

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LIBRARY

APPENDIX II

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AND
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NATURAL GAS COMPOSITION

ARB-TDA- Report No. 60-80B

These data are on file with:

Technology Development and Appraisal Section
Air Resources Branch
Ministry of the Environment
Province of Ontario
880 Bay Street, 4th Floor
Toronto, Ontario M5S 1Z8

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<div> $P_{\text{bar}} = 29.25 \text{ in-Hg}$ Orifice Calibration October 23, 1979 </div>						
T_m	$(V_m)_f$ ft ³	$(V_m)_i$ ft ³	Δt (minutes)	Q_m cfm	$\sqrt{\frac{\Delta H T_m}{M_d P_o}}$	ΔH in-H ₂ O
75 75	1785.00	1783.00	6'-16.9" 6.282	0.318	0.252	0.10
75 78	1788.00	1786.00	3'-40.8" 3.680	0.543	0.436	0.30
79 80	1795.00	1792.00	4'-21.8" 4.363	0.688	0.564	0.50
81 84	1799.00	1796.00	3'-44.2" 3.737	0.803	0.671	0.70
85 86	1803.00	1800.00	3'-11.8" 3.197	0.938	0.782	0.95

TABLE I.1: Calibration of Sampling Train Orifice Meter

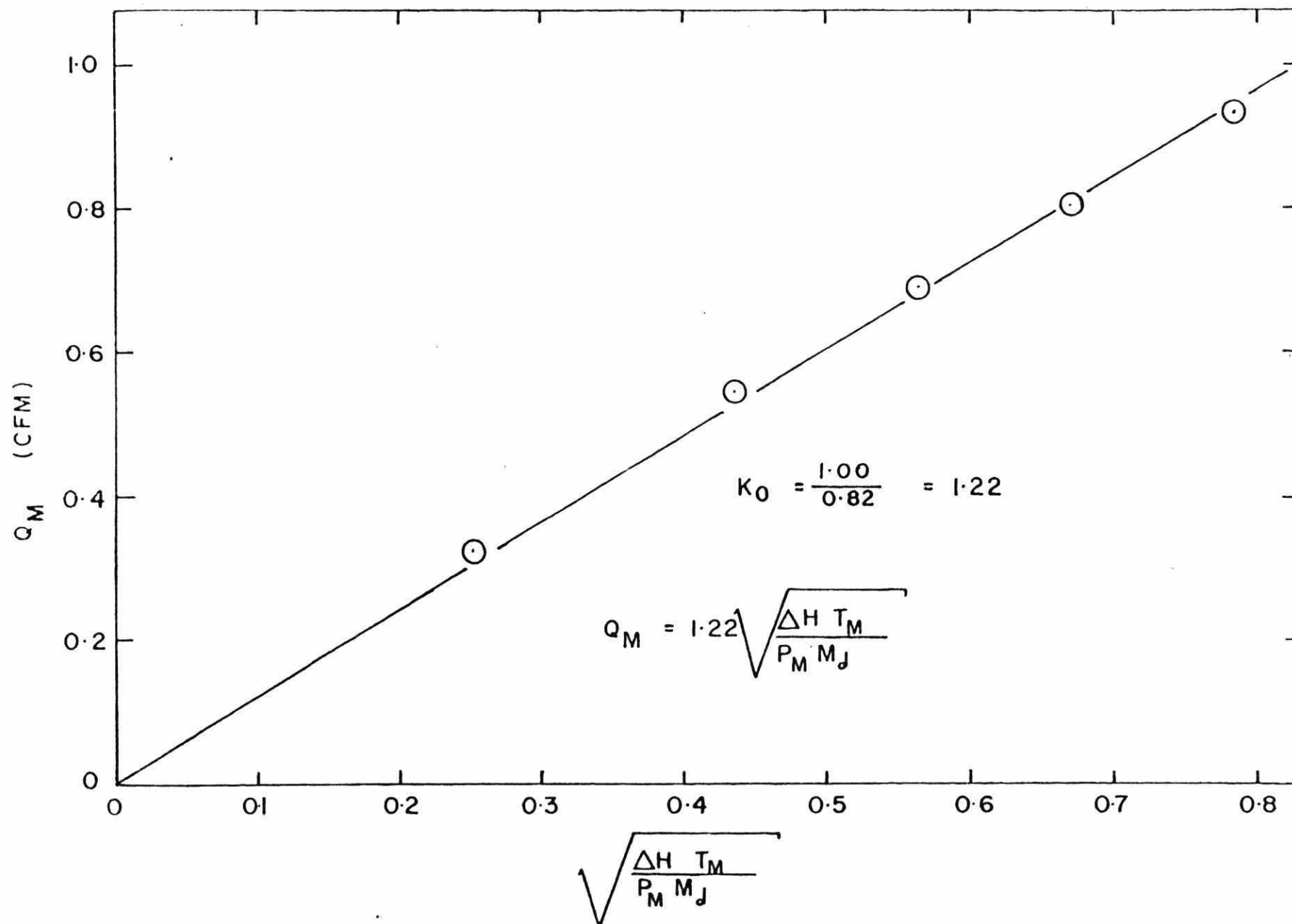


FIGURE I.1: Evaluation of Orifice Meter Constant

Teflon lined probe - October 23, 1979

$C_v Wt = 0.752$

1/4" Nozzle	RPM	$\Delta P_{Wt.}$	ΔP	$\sqrt{\frac{\Delta P}{\Delta P_{Wt.}}}$	C_v	\bar{C}_v
	300	0.0875	0.1085	0.898	0.675	0.671 \pm 0.003
	400	0.1655	0.2055	0.897	0.675	
	550	0.3380	0.4260	0.891	0.670	
	700	0.5870	0.7400	0.891	0.670	
	850	0.8800	1.1140	0.889	0.668	
	1000	1.2380	1.5620	0.890	0.669	
	1100	1.5320	1.9240	0.892	0.671	
3/8" Nozzle	300	0.0930	0.1195	0.882	0.663	0.659 \pm 0.003
	400	0.1680	0.2165	0.881	0.662	
	550	0.3500	0.4540	0.878	0.660	
	700	0.5780	0.7590	0.873	0.656	
	850	0.9000	1.1740	0.876	0.658	
	1000	1.2320	1.6040	0.876	0.659	
	1100	1.4980	1.9640	0.873	0.657	
1/2" Nozzle	300	0.0890	0.11850	0.867	0.652	0.655 \pm 0.003
	400	0.1705	0.22050	0.879	0.661	
	550	0.3440	0.45000	0.874	0.661	
	700	0.5780	0.76000	0.872	0.656	
	850	0.8680	1.13800	0.873	0.657	
	1000	1.2020	1.59800	0.867	0.652	
	1100	1.4220	1.89400	0.866	0.652	

TABLE I.2: Calibration of S-Type Pitot Tube-Sampling Probe Combination

APPENDIX II

TEST DATA
AND
CALCULATIONS

PLANT MODEL 2165-D ACE GRAIN
DRYER

BAROMETRIC PRESSURE (IN. Hg.) 29.47

STACK PRESSURE (IN. H₂O)

LOCATION NEWBURY, ONTARIO

MOISTURE CONTENT VOL. %

TEST 1

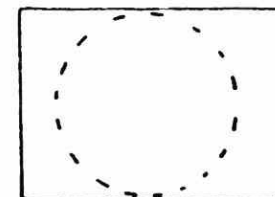
NOZZLE DIA. IN. 0.25

DATE OCT. 26 / 79

PROBE LENGTH 4 EFFECTIVE

AMBIENT TEMPERATURE °F. 39

OPERATORS D.S., C.S.T.P., A.W.G.



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	88				1803.40	255	240	100	165	40	1.0
A-F-1	2.5	88	0.05	10.33	0.04	1803.93	260	225	85	185	40	1.0
2	5.0	88	0.01	4.62	0.008	1804.16	255	235	90	200	40	1.0
3	7.5	88	0.01	4.62	0.008	1804.40	250	235	90	205	40	1.0
4	10.0	88	0.01	4.62	0.008	1804.62	245	245	87	210	40	1.0
5	12.5	88	0.01	4.62	0.008	1804.85	240	250	90	210	40	1.0
6	15.0	88	0.01	4.62	0.008	1805.07	245	255	90	210	40	1.0
	0	88				1806.44	240	250	85	210	40	2.0
A-M-1	2.5	88	0.26	23.56	0.21	1807.66	245	250	85	210	40	2.0
2	5.0	88	0.265	23.79	0.22	1808.87	245	250	70	210	45	2.5
3	7.5	88	0.27	24.01	0.22	1810.12	250	250	70	215	45	2.5
4	10.0	88	0.14	17.29	0.11	1811.02	250	260	70	225	45	2.0
5	12.5	88	0.25	23.11	0.2	1812.10	255	260	75	230	45	2.2
6	15.0	88	0.195	20.41	0.16	1813.08	260	270	80	245	45	2.1
TOTAL	AVERAGE		AV.			TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

PLANT _____

BAROMETRIC PRESSURE (IN. Hg.) _____

STACK PRESSURE (IN. H₂O) _____

LOCATION _____

MOISTURE CONTENT VOL. % _____

TEST 1 _____

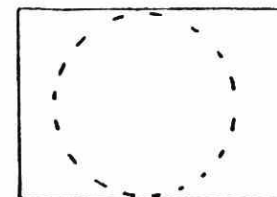
NOZZLE DIA. IN. _____

DATE OCT. 26 / 79 _____

PROBE LENGTH _____

AMBIENT TEMPERATURE °F. _____

OPERATORS _____



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	88				1813.27	260					
A-01	2.5	88	0.47	31.68	0.38	1814.87	260	260	90	230	48	4.5
2	5.0	88	0.47	31.68	0.38	1816.49	260	260	70	240	48	4.5
3	7.5	88	0.49	32.35	0.40	1818.13	255	255	80	240	50	4.5
4	10.0	88	0.49	32.35	0.40	1819.80	255	250	80	235	50	4.5
5	12.5	88	0.49	32.35	0.40	1821.44	250	250	82	232	50	4.5
6	15.0	88	0.43	30.30	0.35	1822.97	255	250	85	230	50	4.0
	TOTAL	AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

PLANT _____

BAROMETRIC PRESSURE (IN. Hg.) _____

STACK PRESSURE (IN. H₂O) _____

LOCATION _____

MOISTURE CONTENT VOL. % _____

TEST 1

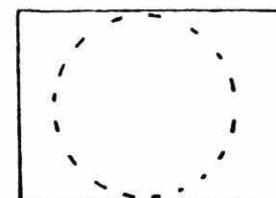
NOZZLE DIA. IN. _____

DATE OCT. 26 / 79

PROBE LENGTH _____

AMBIENT TEMPERATURE °F. _____

OPERATORS _____



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	85°				1823.47	250	235	65	145	50	1.0
B-T-1	2.5	85	0.01	4.61	0.008	1823.69	245	235	65	145	50	1.0
2	5.0	85	0.012	5.05	0.008	1823.92	240	240	62	180	50	1.0
3	7.5	85	0.01	4.61	0.008	1824.15	235	240	62	190	50	1.0
4	10.0	85	0.01	4.61	0.008	1824.37	235	240	65	200	50	1.0
5	12.5	85	0.01	4.61	0.008	1824.60	240	242	65	205	50	1.0
6	15.0	85	0.015	5.64	0.008	1824.85	245	245	62	202	50	1.0
	0	85				1825.66	245	250	60	185	50	4.0
B-1-1	2.5	85	0.30	25.24	0.24	1826.98	245	250	60	185	50	4.0
2	5.0	85	0.19	20.09	0.15	1828.02	250	250	57	210	52	3.0
3	7.5	85	0.23	22.10	0.19	1829.18	255	250	55	210	50	3.2
4	10.0	85	0.24	22.58	0.20	1830.36	250	250	57	212	51	3.2
5	12.5	85	0.23	22.10	0.19	1831.48	255	252	60	215	52	3.1
6	15.0	85	0.24	22.58	0.20	1832.63	250	252	61	220	52	3.1
	TOTAL	AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

PLANT _____

BAROMETRIC PRESSURE (IN. Hg.) _____

STACK PRESSURE (IN. H₂O) _____

LOCATION _____

MOISTURE CONTENT VOL. % _____

TEST 1

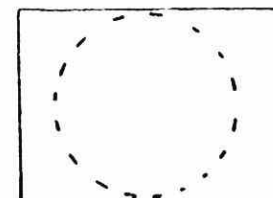
NOZZLE DIA. IN. _____

DATE OCT. 26 / 79

PROBE LENGTH _____

AMBIENT TEMPERATURE °F. _____

OPERATORS _____



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	85				1832.89	260	250	62	202	55	6.0
B0-1	2.5	85	0.60	35.70	0.49	1834.70	265	250	62	202	55	6.0
2	5.0	85	0.60	35.70	0.50	1836.52	260	250	62	210	55	6.0
3	7.5	85	0.61	36.00	0.51	1838.35	255	260	60	220	55	7.0
4	10.0	85	0.55	34.18	0.46	1840.10	250	258	62	225	55	6.5
5	12.5	85	0.50	32.59	0.42	1841.78	250	255	65	230	55	5.5
6	15.0	85	0.45	30.92	0.37	1843.38	245	255	70	230	55	5.0
TOTAL		AVERAGE		AV.	TOTAL			AVERAGE		AV.		

PARTICULATE SAMPLING DATA

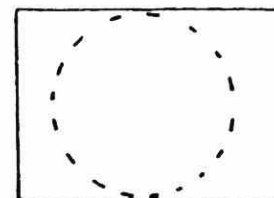
STACK PRESSURE (IN. H₂O) _____

MOISTURE CONTENT VOL. %

NOZZLE DIA. IN.

PROBE LENGTH _____

OPERATORS



TEST TRAVERSES

[illegible]

PARTICULATE SAMPLING DATA

PLANT _____

BAROMETRIC PRESSURE (IN. Hg.) _____

STACK PRESSURE (IN. H₂O) _____

LOCATION _____

MOISTURE CONTENT VOL. % _____

TEST 1

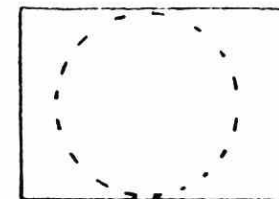
NOZZLE DIA. IN. _____

DATE OCT. 26 / 79

PROBE LENGTH _____

AMBIENT TEMPERATURE °F. _____

OPERATORS _____



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	85				1853.66	260	255	92	210	55	4.5
C-1	2.5	85	0.55	34.18	0.45	1855.41	255	255	92	210	55	4.5
2	5.0	85	0.54	33.87	0.44	1857.10	250	265	78	235	52	4.5
3	7.5	85	0.50	32.59	0.40	1858.78	245	255	80	235	53	4.3
4	10.0	85	0.48	31.93	0.39	1860.39	245	260	84	235	51	4.2
5	12.5	85	0.50	32.59	0.40	1862.01	245	258	83	227	53	4.3
6	15.0	85	0.50	32.59	0.40	1863.66	240	260	85	232	55	4.3
TOTAL		AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

Absolute stack gas pressure in in. Hg. is

$$P_s = P_{bar} + \frac{P_{static} \text{ in. H}_2\text{O}}{13.6 \text{ in. H}_2\text{O/in. Hg.}}$$

$$P_s = \frac{29.47}{13.6} + \frac{0.04}{13.6}$$

$$P_s = \underline{29.47} \text{ in. Hg.}$$

The molecular weight of the stack gas on a dry basis in lb/lb.mole. is

$$M_d = 0.44 (\% \text{ CO}_2) \text{ avg.} + 0.32 (\% \text{ O}_2) \text{ avg.} + 0.28 [(\% \text{ N}_2) \text{ avg.} + (\% \text{ CO}) \text{ avg.}]$$

$$M_d = 0.44 \times \underline{0.4} + 0.32 \times \underline{20.8} + 0.28 (\underline{78.0} + \underline{\quad\quad\quad})$$

+ 0.4 x 0.9 Argon

$$M_d = \underline{0.176} + \underline{6.656} + \underline{21.84} + 0.36$$

$$M_d = \underline{28.932} \text{ lb/lb.mole.}$$

The volume of water vapour collected at reference conditions in ft^3 is

$$V_{wc} = 0.0474 \text{ ft}^3/\text{ml} \times \text{volume of moisture collected ml.}$$

$$V_{wc} = 0.0474 \times \underline{42.66}$$

$$V_{wc} = \underline{2.022} \text{ ft}^3$$

The average ΔP orifice in in. H_2O is

$$\Delta P \text{ orifice avg.} = \frac{\Sigma \Delta P \text{ orifice}}{\# \text{ points}}$$

$$\Delta P \text{ orifice avg.} = \frac{\underline{11.276}}{\underline{54}}$$

$$\Delta P \text{ orifice avg.} = \underline{0.209} \text{ in. H}_2\text{O}$$

The pressure at the gas meter in in. Hg. is

$$P_m = P_{\text{bar}} + \frac{\Delta P \text{ orifice avg. in. H}_2\text{O}}{13.6 \text{ in. H}_2\text{O/in. Hg.}}$$

$$P_m = \underline{29.47} + \frac{\underline{0.209}}{\underline{13.6}}$$

$$P_m = \underline{29.47} + \underline{0.015}$$

$$P_m = \underline{29.485} \text{ in. Hg.}$$

The temperature of the total gas meter in $^{\circ}\text{R}$. is

$$T_m = \frac{\text{I meter temp. } ^{\circ}\text{F.}}{\# \text{ points}} + 460$$

$$T_m = \frac{70}{\quad} + 460$$

$$T_m = \underline{530^{\circ}\text{R}} \quad \text{Temp. Compensated}$$

The total volume of gas metered in ft^3 is

$$V_m = V_f - V_i$$

$$V_m = \underline{\quad} - \underline{\quad}$$

$$V_m = \underline{55.60} \text{ ft}^3$$

The dry gas volume at reference conditions in ft^3 is

$$V_{mc} = 17.71 \frac{^{\circ}\text{R}}{\text{in. Hg.}} \frac{V_m \text{ ft}^3 \times P_m \text{ in. Hg.}}{T_m ^{\circ}\text{R}}$$

$$V_{mc} = 17.71 \times \frac{55.6 \times 29.485}{530}$$

$$V_{mc} = \underline{54.78} \text{ ft}^3$$

The stack gas moisture content, i.e. the proportion by volume of water vapour in the gas stream is

$$B_{wo} = \frac{V_{wc} \text{ ft}^3}{V_{wc} \text{ ft}^3 + V_{mc} \text{ ft}^3} \quad (\text{using dry-rite})$$

$$B_{wo} = \frac{2.022}{2.022 + 54.78}$$

$$B_{wo} = \frac{2.022}{56.802}$$

$$B_{wo} = \underline{0.0356}$$

The molecular weight of the stack gas on a wet basis in lb/lb mole. is

$$M_s = M_d \text{ lb/lb mole } (1 - B_{wo}) + 18 \text{ lb/lb mole } \times B_{wo}$$

$$M_s = \underline{28.932} \times (1 - \underline{0.0356}) + 18 \times \underline{0.0356}$$

$$M_s = \underline{28.932} \times \underline{0.9644} + \underline{0.6408}$$

$$M_s = \underline{27.902} + \underline{0.6408}$$

$$M_s = \underline{28.543} \text{ lb/lb mole.}$$

The average velocity of the stack in ft/sec is

$$U_s = \frac{\Sigma V}{\# \text{ points}}$$

$$U_s = \frac{1093.07}{54}$$

$$U_s = \underline{20.24} \text{ ft/sec}$$

The average temperature of the stack in °R. is

$$T_s \text{ avg.} = \frac{\Sigma T_s}{\# \text{ points}} + 460$$

$$T_s \text{ avg.} = \frac{5418}{63} + 460$$

$$T_s \text{ avg.} = \underline{86} + 460$$

$$T_s \text{ avg.} = \underline{546} \text{ °R.}$$

The cross-sectional area of the stack in ft^2 is

$$A_s = \frac{\pi D^2}{4}$$

$$A_s = \frac{\pi}{4} \times (\text{_____})^2$$

$$A_s = 0.7854 \times \text{_____}$$

$$A_s = \underline{9} \text{ ft}^2 / \text{FILTER DRUM}$$

The volumetric stack gas flowrate on a dry basis at reference conditions in ft^3/hr is

$$Q_s = 3600 \text{ sec/hr} \times U_s \text{ ft/sec} \times A_s \text{ ft}^2 \times (1 - B_{wO}) \\ \times \frac{T_{\text{ref}}}{T_{s \text{ avg.}}} \times \frac{P_s}{P_{\text{ref}}}$$

$$Q_s = 3600 \times \underline{20.24} \text{ ft/sec} \times \underline{9} \text{ ft}^2 \times (1 - \underline{0.0356}) \\ \times \frac{530}{546^\circ\text{R}} \times \frac{29.47 \text{ in. Hg.}}{29.92 \text{ in. Hg.}}$$

$$Q_s = 3600 \times \underline{20.24} \times \underline{9} \times \underline{0.9644} \times \underline{0.9707} \times \underline{0.9850}$$

$$Q_s = \underline{6.047 \times 10^5} \text{ ft}^3/\text{hr} / \text{FILTER DRUM}$$

The total amount of particulate matter collected in mg. is

$$M_p = \underline{11.7} \text{ mg.}$$

The concentration of particulate matter in stack gas on a dry basis at reference conditions in lb/ft^3 is

$$C_p = 2.205 \times 10^{-6} \text{ lb/mg} \times \frac{M_p}{V_{mc}}$$

$$C_p = 2.205 \times 10^{-6} \times \frac{11.7 \text{ mg}}{54.78 \text{ ft}^3}$$

$$C_p = \underline{4.709 \times 10^{-7}} \text{ lb/ft}^3$$

The emission rate of particulate matter from the stack on a dry basis at reference conditions in lb/hr is

$$ER_p = C_p \text{ lb/ft}^3 \times Q_s \text{ ft}^3/\text{hr}$$

$$ER_p = \underline{4.709 \times 10^{-7}} \times \underline{6.047 \times 10^5}$$

$$ER_p = \underline{0.285} \text{ lb/hr / FILTER DRUM}$$

$$= 0.855 \text{ lb/hr Total}$$

PLANT GRAIN DRYERDATE OCTOBER 26 1979LOCATION NEW BURY, ONTARIO

OPERATORS _____

TEST 1

ANALYST _____

MOISTURE DATA

	FINAL WEIGHT (gm.)	TARE WEIGHT (gm.)	HEIGHT OF MOISTURE (gm.)
IMPINGER # 1	641.5	621.92	19.52
IMPINGER # 2	613.9	604.25	7.05
IMPINGER # 3	441.2	439.81	1.39
IMPINGER # 4	683.5	670.86	12.64
TOTAL			42.66
MOISTURE VOLUME			42.66 ml.

PARTICULATE DATA

	FINAL WEIGHT (gm.)	TARE WEIGHT (gm.)	WEIGHT OF PARTICULATE (gm.)
FILTER	0.7527	0.7526	0.0001
BEAKER WITH (PROBE - NOZZLE - CYCLONE) WASHINGS	49.3568	49.3503	0.0051
CYCLONE FLASK	48.6537	48.6472	0.0065
BEAKER WITH (IMPINGER FILTER-HOLDER) CONTENTS AND WASHINGS	47.7275	47.7275	0.0000
TOTAL (gm.)			0.0117
PARTICULATES IN (mg.)			11.7

MODEL 2165-D
PLANT ACE CANN ONTARIO

BAROMETRIC PRESSURE (IN. Hg.) 29.47

STACK PRESSURE (IN. H₂O) _____

LOCATION NEWBURY, ONTARIO MOISTURE CONTENT VOL. % _____

TEST 2

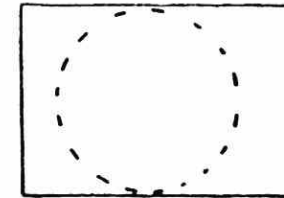
NOZZLE DIA. IN. 0.250

DATE OCTOBER 26, 1979

PROBE LENGTH 4' EXPOSED

AMBIENT TEMPERATURE °F. 42

OPERATORS AWG, VS, CSP



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	87				1870.00	235	225	42	75	40	—
DT-1	2.5	87	0.02	6.53	0.016	1870.33	240	225	43	122	42	0.5
2	5.0	85	0.01	4.61	0.008	1870.56	242	222	45	140	45	0.5
3	7.5	85	0.013	5.25	0.008	1870.82	248	240	45	145	45	0.5
4	10.0	87	0.01	4.62	0.008	1871.06	245	230	45	155	45	0.5
5	12.5	87	0.01	4.62	0.008	1871.28	241	232	45	160	43	0.5
6	15.0	87	0.01	4.62	0.008	1871.51	235	260	42	160	49	0.5
	0	86				1871.51	240	262	42	140	49	—
DM-1	2.5	86	0.30	25.26	0.23	1872.73	245	215	42	145	50	0.5
2	5.0	86	0.265	23.74	0.21	1873.90	250	210	40	154	50	0.5
3	7.5	86	0.27	23.96	0.22	1875.07	253	212	42	175	51	0.5
4	10.0	87	0.22	21.65	0.17	1876.16	255	210	41	183	51	0.5
5	12.5	87	0.29	24.86	0.23	1877.43	252	210	44	140	52	0.5
6	15.0	87	0.20	20.64	0.16	1878.43	250	265	44	187	55	0.5
	TOTAL	AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PLANT _____

BAROMETRIC PRESSURE (IN. Hg.) 29.47 STACK PRESSURE (IN. H₂O) _____

LOCATION _____

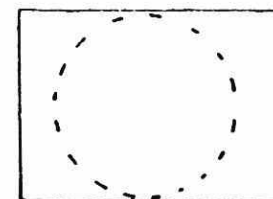
MOISTURE CONTENT VOL. % _____

TEST 2NOZZLE DIA. IN. 0.250DATE OCTOBER 26, 1979

PROBE LENGTH _____

AMBIENT TEMPERATURE °F. _____

OPERATORS _____



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	87				1878.43	270	240	14	150	55	—
DB-1	2.5	87	0.57	34.85	0.46	1880.15	272	245	14	160	55	4.8
2	5.0	87	0.60	35.75	0.49	1881.91	275	250	45	195	58	5.0
3	7.5	87	0.58	35.15	0.48	1883.65	272	255	45	200	57	4.8
4	10.0	87	0.62	36.34	0.51	1885.39	270	255	45	197	57	5.2
5	12.5	87	0.59	35.45	0.48	1887.22	270	255	46	205	58	4.7
6	15.0	87	0.55	34.23	0.45	1888.94	270	255	45	202	60	4.5
	0	87				1890.01	240	285	70	120	55	—
FT-1	2.5	87	0.02	6.53	0.016	1890.34	245	285	70	145	58	1.0
2	5.0	87	0.02	6.53	0.016	1890.66	250	280	55	110	58	1.0
3	7.5	87	0.015	5.65	0.01	1890.95	255	275	52	197	57	1.0
4	10.0	87	0.01	4.62	0.008	1891.18	260	275	52	210	57	1.0
5	12.5	87	0.01	4.62	0.008	1891.40	260	275	55	210	57	1.0
6	15.0	87	0.01	4.62	0.008	1891.63	255	270	55	215	57	1.0
	TOTAL	AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

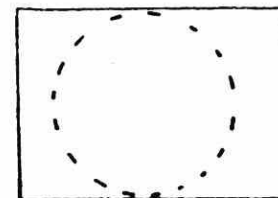
STACK PRESSURE (IN. H₂O) _____

MOISTURE CONTENT VOL. %

NOZZLE DIA. IN. 0.250

PROBE LENGTH _____

OPERATORS



TEST TRAVERSES

15
(3)

PARTICULATE SAMPLING DATA

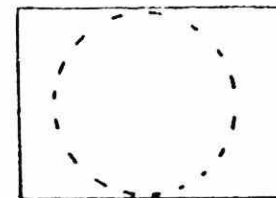
STACK PRESSURE (IN. H₂O) _____

MOISTURE CONTENT VOL. % _____

NOZZLE DIA. IN. 0.250

PROBE LENGTH _____

OPERATORS



TEST TRAVERSES

9.4.

PARTICULATE SAMPLING DATA

PLANT _____

BAROMETRIC PRESSURE (IN. Hg.) 29.42STACK PRESSURE (IN. H₂O) _____

LOCATION _____

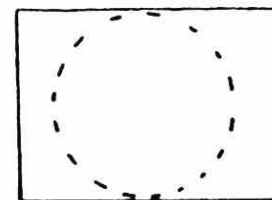
MOISTURE CONTENT VOL. % _____

TEST 2NOZZLE DIA. IN. 0.250DATE October 26, 1979

PROBE LENGTH _____

AMBIENT TEMPERATURE °F. _____

OPERATORS _____



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	93				1918.96	260	250	45	170	55	—
1B-1	2.5	93	0.58	35.34	0.47	1920.73	260	250	42	175	55	5.0
2	5.0	93	0.58	35.34	0.48	1922.47	265	255	41	180	55	5.1
3	7.5	93	0.55	34.42	0.46	1924.14	270	260	40	185	55	4.8
4	10.0	93	0.62	36.59	0.51	1925.94	270	260	40	185	56	5.5
5	12.5	93	0.60	35.95	0.49	1927.69	275	255	40	190	56	5.5
6	15.0	93	0.52	33.46	0.43	1929.38	280	250	40	180	56	7.7
TOTAL		AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

The volume of water vapour collected at reference conditions in ft^3 is

$$V_{wc} = 0.0474 \text{ ft}^3/\text{ml} \times \text{volume of moisture collected ml.}$$

$$V_{wc} = 0.0474 \times \underline{43.6}$$

$$V_{wc} = \underline{2.069} \text{ ft}^3$$

The average ΔP orifice in in. H_2O is

$$\Delta P \text{ orifice avg.} = \frac{\Sigma \Delta P \text{ orifice}}{\# \text{ points}}$$

$$\Delta P \text{ orifice avg.} = \frac{\underline{12.573}}{\underline{54}}$$

$$\Delta P \text{ orifice avg.} = \underline{0.233} \text{ in. H}_2\text{O}$$

The pressure at the gas meter in in. Hg. is

$$P_m = P_{bar} + \frac{\Delta P \text{ orifice avg. in. H}_2\text{O}}{13.6 \text{ in. H}_2\text{O/in. Hg.}}$$

$$P_m = \underline{29.47} + \frac{\underline{0.233}}{\underline{13.6}}$$

$$P_m = \underline{29.47} + \underline{0.017}$$

$$P_m = \underline{29.49} \text{ in. Hg.}$$

Absolute stack gas pressure in in. Hg. is

$$P_s = P_{bar} + \frac{P_{static} \text{ in. H}_2\text{O}}{13.6 \text{ in. H}_2\text{O/in. Hg.}}$$

$$P_s = \underline{29.47} + \frac{\underline{0.04}}{13.6}$$

$$P_s = \underline{29.47} \text{ in. Hg.}$$

The molecular weight of the stack gas on a dry basis in lb/lb.mole. is

$$M_d = 0.44 (\% \text{ CO}_2) \text{ avg.} + 0.32 (\% \text{ O}_2) \text{ avg.} + 0.28 [(\% \text{ N}_2) \text{ avg.} + (\% \text{ CO}) \text{ avg.}]$$

$$M_d = 0.44 \times \underline{0.4} + 0.32 \times \underline{20.7} + 0.28 (\underline{78.0} + \underline{0})$$

$$M_d = \underline{0.176} + \underline{6.624} + \underline{21.84} + \overset{+(0.44)(0.9)}{0.36}$$

$$M_d = \underline{29.00} \text{ lb/lb.mole.}$$

The temperature of the total gas meter in $^{\circ}\text{R}$. is

$$T_m = \frac{\text{meter temp. } ^{\circ}\text{F.}}{\text{\# points}} + 460$$

$$T_m = \underline{\hspace{2cm}} + 460$$

$$T_m = \underline{530^{\circ}\text{R}} \quad (\text{TEMPERATURE CORRECTION})$$

The total volume of gas metered in ft^3 is

$$V_m = V_f - V_i$$

$$V_m = \underline{\hspace{2cm}} - \underline{\hspace{2cm}}$$

$$V_m = \underline{56.70} \text{ ft}^3$$

The dry gas volume at reference conditions in ft^3 is

$$V_{mc} = 17.71 \frac{^{\circ}\text{R}}{\text{in. Hg.}} \frac{V_m \text{ ft}^3 \times P_m \text{ in. Hg.}}{T_m ^{\circ}\text{R}}$$

$$V_{mc} = 17.71 \times \frac{56.70 \times 29.49}{530}$$

$$V_{mc} = \underline{55.87} \text{ ft}^3$$

The stack gas moisture content, i.e. the proportion by volume of water vapour in the gas stream is

$$B_{wo} = \frac{V_{wc} \text{ ft}^3}{V_{wc} \text{ ft}^3 + V_{mo} \text{ ft}^3} \quad (\text{using dry-basis})$$

$$B_{wo} = \frac{2.304}{2.304 + 55.87}$$

$$B_{wo} = \underline{\hspace{2cm}}$$

$$B_{wo} = \underline{0.0396}$$

The molecular weight of the stack gas on a wet basis in lb/lb mole. is

$$M_s = M_d \text{ lb/lb mole} (1 - B_{wo}) + 18 \text{ lb/lb mole} \times B_{wo}$$

$$M_s = \underline{29.00} \times (1 - \underline{0.0396}) + 18 \times \underline{0.0396}$$

$$M_s = \underline{29.00} \times \underline{0.9604} + \underline{0.713}$$

$$M_s = \underline{27.85} + \underline{0.713}$$

$$M_s = \underline{28.56} \text{ lb/lb mole.}$$

The average velocity of the stack in ft/sec is

$$U_s = \frac{\sum V}{\# \text{ points}}$$

$$U_s = \frac{1150.57}{54}$$

$$U_s = \underline{21.31} \text{ ft/sec}$$

The average temperature of the stack in °R. is

$$T_s \text{ avg.} = \frac{\sum T_s}{\# \text{ points}} + 460$$

$$T_s \text{ avg.} = \frac{4819}{54} + 460$$

$$T_s \text{ avg.} = \underline{89.2} + 460$$

$$T_s \text{ avg.} = \underline{549.2}^{\circ}\text{R.}$$

The cross-sectional area of the stack in ft^2 is

$$A_s = \frac{\pi D^2}{4}$$

$$A_s = \frac{\pi}{4} \times (\text{_____})^2$$

$$A_s = 0.7854 \times \text{_____}$$

$$A_s = \underline{9.0} \text{ ft}^2 / \text{FILTER DRUM}$$

The volumetric stack gas flowrate on a dry basis at reference conditions in ft^3/hr is

$$Q_s = 3600 \text{ sec/hr} \times U_s \text{ ft/sec} \times A_s \text{ ft}^2 \times (1 - B_{wO}) \times \frac{T_{\text{ref}}}{T_{s \text{ avg.}}} \times \frac{P_s}{P_{\text{ref}}}$$

$$Q_s = 3600 \times \underline{21.31} \text{ ft/sec} \times \underline{9.0} \text{ ft}^2 \times (1 - \underline{0.0396}) \times \frac{549.2}{549.2} \times \frac{29.47 \text{ in. Hg.}}{29.92 \text{ in. Hg.}}$$

$$Q_s = 3600 \times \underline{21.31} \times \underline{9.0} \times \underline{0.9604} \times \underline{0.9650} \times \underline{0.9250}$$

$$Q_s = \underline{6.30 \times 10^5} \text{ ft}^3/\text{hr} / \text{FILTER DRUM}$$

$$\underline{1.89 \times 10^6} \text{ ft}^3/\text{hr} \text{ TOTAL}$$

The total amount of particulate matter collected in mg. is

$$M_p = \underline{12.6} \text{ mg.}$$

The concentration of particulate matter in stack gas on a dry basis at reference conditions in lb/ft³ is

$$C_p = 2.205 \times 10^{-6} \text{ lb/mg} \times \frac{M_p}{V_{mc}}$$

$$C_p = 2.205 \times 10^{-6} \times \frac{12.6 \text{ mg}}{55.87 \text{ ft}^3}$$

$$C_p = \underline{4.97 \times 10^{-7}} \text{ lb/ft}^3$$

The emission rate of particulate matter from the stack on a dry basis at reference conditions in lb/hr is

$$ER_p = C_p \text{ lb/ft}^3 \times Q_s \text{ ft}^3/\text{hr}$$

$$ER_p = \underline{4.97 \times 10^{-7}} \times \underline{6.30 \times 10^5}$$

$$ER_p = \underline{0.313} \text{ lb/hr / FILTER DRUM}$$

$$= \underline{0.939} \text{ lb/hr TOTAL}$$

PLANT GRAND DRYERDATE OCTOBER 26, 1977LOCATION NEWBURY

OPERATORS _____

TEST 2

ANALYST _____

MOISTURE DATA

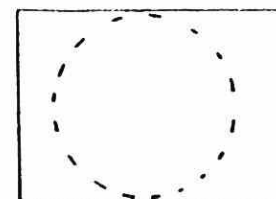
	FINAL WEIGHT (gm.)	TARE WEIGHT (gm.)	WEIGHT OF MOISTURE (gm.)
IMPINGER # 1	680.3	651.3	29.0
IMPINGER # 2	624.5	616.6	7.9
IMPINGER # 3	446.8	442.6	4.2
IMPINGER # 4	693.5	686.0	7.5
TOTAL			48.6
MOISTURE VOLUME			48.6 ml.

PARTICULATE DATA

	FINAL WEIGHT (gm.)	TARE WEIGHT (gm.)	WEIGHT OF PARTICULATE (gm.)
FILTER	0.7631	0.7630	0.0001
BEAKER WITH (PROBE - NOZZLE - CYCLONE) WASHINGS	50.9446	50.9402	0.0044
CYCLONE FLASK	47.4063	47.3982	0.0081
BEAKER WITH (IMPINGER, FILTER-HOLDER) CONTENTS AND WASHINGS	47.8870	47.8872	0.0000
TOTAL (gm.)			0.0126
PARTICULATES IN (mg.)			12.6

PLANT MODEL 2165-D ACE GRAIN DRYERBAROMETRIC PRESSURE (IN. Hg.) 29.53STACK PRESSURE (IN. H₂O) _____LOCATION NEWBURY, ONTARIO

MOISTURE CONTENT VOL. % _____

TEST TEST 3NOZZLE DIA. IN. 0.25DATE OCT. 27 / 79PROBE LENGTH 4' EFFECTIVEAMBIENT TEMPERATURE °F. 44OPERATORS D.S., C.S.T.P., A.W.G.

TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	86				1960.02	250	220	35	97	45	0.5
AT-1	2.5	86	0.04	9.20	0.03	1960.49	255	220	35	97	45	0.5
2	5.0	86	0.03	7.97	0.024	1960.91	255	232	40	150	35	0.5
3	7.5	86	0.01	4.60	0.008	1961.15	260	245	48	195	35	0.5
4	10.0	86	0.01	4.60	0.008	1961.38	255	252	56	212	35	0.5
5	12.5	86	0.01	4.60	0.008	1961.61	250	258	62	215	37	0.5
6	15.0	86	0.01	4.60	0.008	1961.85	250	262	65	215	38	0.5
	0	86				1962.94	240	270	70	207	40	2.2
AT-1	2.5	86	0.25	23.01	0.20	1964.15	245	270	70	207	40	2.2
2	5.0	86	0.25	23.01	0.20	1965.35	245	271	59	215	40	2.2
3	7.5	86	0.22	21.58	0.18	1966.48	245	272	58	220	40	2.0
4	10.0	86	0.23	22.07	0.19	1967.62	250	270	59	220	41	2.2
5	12.5	86	0.24	22.54	0.19	1968.77	260	269	59	218	42	2.3
6	15.0	86	0.17	18.97	0.14	1969.76	265	269	60	220	45	2.2
	TOTAL	AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

PLANT _____

BAROMETRIC PRESSURE (IN. Hg.) _____

STACK PRESSURE (IN. H₂O) _____

LOCATION _____

MOISTURE CONTENT VOL. % _____

TEST 3

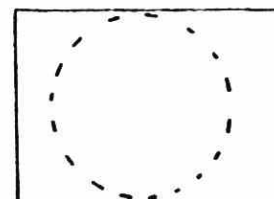
NOZZLE DIA. IN. _____

DATE OCT. 27 / 79

PROBE LENGTH _____

AMBIENT TEMPERATURE °F. _____

OPERATORS _____



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	86				1969.87	260					
AB-1	2.5	86	0.43	30.17	0.35	1971.37	260	270	70	202	45	3.5
2	5.0	86	0.42	29.82	0.34	1972.87	260	268	59	222	45	3.5
3	7.5	86	0.33	26.43	0.27	1974.26	265	265	60	230	47	3.5
4	10.0	86	0.44	30.52	0.36	1975.77	265	252	59	228	47	3.8
5	12.5	86	0.43	30.17	0.35	1977.31	260	265	59	230	47	3.9
6	15.0	86	0.39	28.73	0.32	1978.77	260	265	59	230	48	3.5
TOTAL		AVERAGE		AV.	TOTAL			AVERAGE		AV.		

PARTICULATE SAMPLING DATA

STACK PRESSURE (IN. H₂O)

MOISTURE CONTENT VOL. %

NOZZLE DIA. IN.

PROBE LENGTH _____

OPERATORS



TEST TRAVERSES

TRANSVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. IN. Hg.)
									OUTLET	INLET		
	0	86				1978.85	270	295	95	185	47	0.5
B-1	2.5	86	0.01	4.60	0.008	1979.07	270	295	95	185	47	0.5
2	5.0	86	0.01	4.60	0.008	1979.30	270	295	90	220	48	0.5
3	7.5	86	0.01	4.60	0.008	1979.54	265	295	85	230	49	0.5
4	10.0	86	0.01	4.60	0.008	1979.78	265	290	80	230	48	0.5
5	12.5	86	0.01	4.60	0.008	1980.01	265	287	80	227	49	0.6
6	15.0	86	0.01	4.60	0.008	1980.24	265	290	78	230	48	0.6
	0	86				1981.44	260	287	80	210	50	6.0
B-1	2.5	86	0.27	23.91	0.22	1982.65	255	287	80	210	50	6.0
2	5.0	86	0.28	24.35	0.23	1983.92	260	287	65	225	50	6.5
3	7.5	86	0.28	24.35	0.23	1985.18	260	285	62	230	50	6.5
4	10.0	86	0.26	23.46	0.21	1985.40	255	280	60	230	50	6.2
5	12.5	86	0.22	21.58	0.18	1987.50	255	275	60	230	51	5.2
6	15.0	86	0.20	20.58	0.16	1988.56	250	280	65	230	52	5.2
	TOTAL	AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

PLANT _____

BAROMETRIC PRESSURE (IN. Hg.) _____

STACK PRESSURE (IN. H₂O) _____

LOCATION _____

MOISTURE CONTENT VOL. % _____

TEST 3

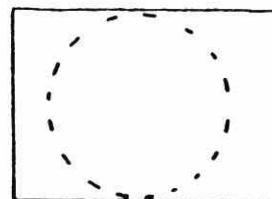
NOZZLE DIA. IN. _____

DATE OCT. 27 / 79

PROBE LENGTH _____

AMBIENT TEMPERATURE °F. _____

OPERATORS _____



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	86				1988.64	230	280	65	220	52	11
BB-1	2.5	86	0.5	32.53	0.41	1990.07	230	280	65	220	52	11
2	5.0	86	0.51	32.86	0.42	1991.51	235	280	65	225	51	11
3	7.5	86	0.50	32.53	0.41	1992.96	240	280	65	230	55	11
4	10.0	86	0.50	32.53	0.42	1994.40	245	270	65	220	55	11.5
5	12.5	86	0.45	30.87	0.37	1995.77	245	270	65	220	55	11.5
6	15.0	86	0.43	30.17	0.36	1997.14	245	270	65	220	55	11.5
	TOTAL	AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

PLANT _____

BAROMETRIC PRESSURE (IN. Hg.) _____

STACK PRESSURE (IN. H₂O) _____

LOCATION _____

MOISTURE CONTENT VOL. % _____

TEST 3

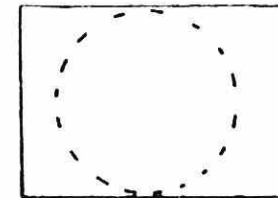
NOZZLE DIA. IN. _____

DATE OCT. 27 / 79

PROBE LENGTH _____

AMBIENT TEMPERATURE °F. _____

OPERATORS _____



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	86				1997.23	245	260	95	185	55	0.5
CT-1	2.5	86	0.1	14.55	0.083	1997.95	245	260	95	185	55	0.5
2	5.0	86	0.1	14.55	0.083	1998.70	245	275	90	220	53	1.0
3	7.5	86	0.1	14.55	0.083	1999.44	240	295	85	242	53	1.0
4	10.0	86	0.05	10.29	0.042	1999.96	245	305	85	255	54	0.8
5	12.5	86	0.05	10.29	0.042	2000.49	250	300	84	250	53	0.8
6	15.0	86	0.05	10.29	0.042	2001.03	250	300	84	250	54	0.8
	0	86				2001.50	255	295	97	200	55	3.0
CH-1	2.5	86	0.23	22.07	0.19	2002.66	255	295	97	200	55	3.0
2	5.0	86	0.20	20.58	0.17	2003.74	260	295	72	235	55	2.6
3	7.5	86	0.25	23.01	0.21	2004.95	260	290	72	235	55	3.0
4	10.0	86	0.20	20.58	0.17	2006.02	260	290	69	235	55	2.6
5	12.5	86	0.27	23.91	0.22	2007.25	265	290	70	235	55	3.0
6	15.0	86	0.22	21.58	0.18	2008.38	260	285	70	235	55	2.7
	TOTAL	AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

PLANT _____

BAROMETRIC PRESSURE (IN. Hg.) _____

STACK PRESSURE (IN. H₂O) _____

LOCATION _____

MOISTURE CONTENT VOL. % _____

TEST 3

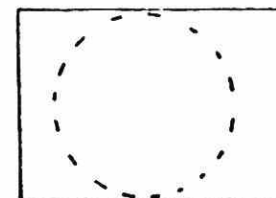
NOZZLE DIA. IN. _____

DATE OCT. 27 / 79

PROBE LENGTH _____

AMBIENT TEMPERATURE °F. _____

OPERATORS _____



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	86				2008.50	255	280	69	170	55	4.7
CO-1	2.5	86	0.5	32.53	0.41	2010.19	255	280	69	170	55	4.7
2	5.0	86	0.5	32.53	0.41	2011.89	250	280	64	215	55	4.5
3	7.5	86	0.4	29.10	0.33	2013.38	245	282	63	225	55	4.3
4	10.0	86	0.26	23.46	0.22	2014.60	240	270	65	225	55	3.6
5	12.5	86	0.3	25.20	0.25	2015.92	240	270	65	225	57	3.2
6	15.0	86	0.38	28.36	0.32	2017.40	235	275	67	225	56	3.7
	TOTAL	AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

Absolute stack gas pressure in in. Hg. is

$$P_s = P_{bar} + \frac{P_{static} \text{ in. H}_2\text{O}}{13.6 \text{ in. H}_2\text{O/in. Hg.}}$$

$$P_s = \underline{29.53} + \frac{\underline{0.04}}{13.6}$$

$$P_s = \underline{29.53} \text{ in. Hg.}$$

The molecular weight of the stack gas on a dry basis in lb/lb.mole. is

$$M_d = 0.44 (\% \text{ CO}_2) \text{ avg.} + 0.32 (\% \text{ O}_2) \text{ avg.} + 0.28 [(\% \text{ N}_2) \text{ avg.} + (\% \text{ CO}) \text{ avg.}]$$

$$M_d = 0.44 \times \underline{0.4} + 0.32 \times \underline{20.8} + 0.28 (\underline{77.9} + \underline{\quad})$$

$$M_d = \underline{0.176} + \underline{6.656} + \underline{21.81} + 0.36$$

$$M_d = \underline{29.002} \text{ lb/lb.mole.}$$

The volume of water vapour collected at reference conditions in ft^3 is

$$V_{wc} = 0.0474 \text{ ft}^3/\text{ml} \times \text{volume of moisture collected ml.}$$

$$V_{wc} = 0.0474 \times \underline{39.3}$$

$$V_{wc} = \underline{1.863} \text{ ft}^3$$

The average ΔP orifice in in. H_2O is

$$\Delta P \text{ orifice avg.} = \frac{\Sigma \Delta P \text{ orifice}}{\# \text{ points}}$$

$$\Delta P \text{ orifice avg.} = \frac{\underline{11.004}}{\underline{54}}$$

$$\Delta P \text{ orifice avg.} = \underline{0.204} \text{ in. H}_2\text{O}$$

The pressure at the gas meter in in. Hg. is

$$P_m = P_{\text{bar}} + \frac{\Delta P \text{ orifice avg. in. H}_2\text{O}}{13.6 \text{ in. H}_2\text{O/in. Hg.}}$$

$$P_m = \underline{29.53} + \frac{\underline{0.204}}{\underline{13.6}}$$

$$P_m = \underline{29.53} + \underline{0.015}$$

$$P_m = \underline{29.545} \text{ in. Hg.}$$

The temperature of the total gas meter in $^{\circ}\text{R}$. is

$$T_m = \frac{\text{L meter temp. } ^{\circ}\text{F.}}{\# \text{ points}} + 460$$

$$T_m = \frac{70}{\quad} + 460$$

$$T_m = \underline{530^{\circ}\text{R}} \quad \text{Temperature Compensated}$$

The total volume of gas metered in ft^3 is

$$V_m = V_f - V_i$$

$$V_m = \underline{\quad} - \underline{\quad}$$

$$V_m = \underline{54.14} \text{ ft}^3$$

The dry gas volume at reference conditions in ft^3 is

$$V_{mc} = 17.71 \frac{^{\circ}\text{R}}{\text{in. Hg.}} \frac{V_m \text{ ft}^3 \times P_m \text{ in. Hg.}}{T_m ^{\circ}\text{R}}$$

$$V_{mc} = 17.71 \times \frac{54.14 \times 29.545}{530}$$

$$V_{mc} = \underline{53.450} \text{ ft}^3$$

The stack gas moisture content, i.e. the proportion by volume of water vapour in the gas stream is

$$B_{wo} = \frac{V_{wc} \text{ ft}^3}{V_{wc} \text{ ft}^3 + V_{mo} \text{ ft}^3} \quad (\text{using dry-basis})$$

$$B_{wo} = \frac{1.863}{1.863 + 53.450}$$

$$B_{wo} = \frac{1.863}{55.314}$$

$$B_{wo} = \underline{0.0337}$$

The molecular weight of the stack gas on a wet basis in lb/lb mole. is

$$M_s = M_d \text{ lb/lb mole } (1 - B_{wo}) + 18 \text{ lb/lb mole } \times B_{wo}$$

$$M_s = \underline{29.002} \times (1 - \underline{0.0337}) + 18 \times \underline{0.0337}$$

$$M_s = \underline{29.002} \times \underline{0.9663} + \underline{0.6066}$$

$$M_s = \underline{28.025} + \underline{0.6066}$$

$$M_s = \underline{28.632} \text{ lb/lb mole.}$$

The average velocity of the stack in ft/sec is

$$U_s = \frac{\sum V}{\# \text{ points}}$$

$$U_s = \frac{1057.34}{54}$$

$$U_s = \underline{19.58} \text{ ft/sec}$$

The average temperature of the stack in °R. is

$$T_s \text{ avg.} = \frac{\sum T_s}{\# \text{ points}} + 460$$

$$T_s \text{ avg.} = \frac{5418}{63} + 460$$

$$T_s \text{ avg.} = \underline{86} + 460$$

$$T_s \text{ avg.} = \underline{546} \text{ °R.}$$

The cross-sectional area of the stack in ft^2 is

$$A_s = \frac{\pi D^2 \text{ft}^2}{4}$$

$$A_s = \frac{\pi}{4} \times (\text{_____})^2$$

$$A_s = 0.7854 \times \text{_____}$$

$$A_s = \underline{9} \text{ ft}^2 / \text{FILTER DRUM}$$

The volumetric stack gas flowrate on a dry basis at reference conditions in ft^3/hr is

$$Q_s = 3600 \text{ sec/hr} \times U_s \text{ ft/sec} \times A_s \text{ ft}^2 \times (1 - B_{wO})$$

$$\times \frac{T_{\text{ref}}}{T_{s \text{ avg.}}} \times \frac{P_s}{P_{\text{ref}}}$$

$$Q_s = 3600 \times \underline{19.58} \text{ ft/sec} \times \underline{9} \text{ ft}^2 \times (1 - \underline{0.0337})$$

$$\times \frac{\underline{530}}{\underline{546}^\circ\text{R}} \times \frac{\underline{29.53 \text{ in. Hg.}}}{\underline{29.92 \text{ in. Hg.}}}$$

$$Q_s = 3600 \times \underline{19.58} \times \underline{9} \times \underline{0.9663} \times \underline{0.9707} \times \underline{0.9870}$$

$$Q_s = \underline{5.873 \times 10^5} \text{ ft}^3/\text{hr} / \text{FILTER DRUM}$$

The total amount of particulate matter collected in mg. is

$$M_p = \underline{10.8} \text{ mg.}$$

The concentration of particulate matter in stack gas on a dry basis at reference conditions in lb/ft^3 is

$$C_p = 2.205 \times 10^{-6} \text{ lb/mg} \times \frac{M_p}{V_{mc}}$$

$$C_p = 2.205 \times 10^{-6} \times \frac{10.8 \text{ mg}}{53.450 \text{ ft}^3}$$

$$C_p = \underline{4.455 \times 10^{-7}} \text{ lb/ft}^3$$

The emission rate of particulate matter from the stack on a dry basis at reference conditions in lb/hr is

$$ER_p = C_p \text{ lb/ft}^3 \times Q_s \text{ ft}^3/\text{hr}$$

$$ER_p = \underline{4.455 \times 10^{-7}} \times \underline{51.873 \times 10^5}$$

$$ER_p = \underline{0.262} \text{ lb/hr / FILTER DRUM}$$
$$= 0.786 \text{ lb/hr Total}$$

PLANT GRAN DRILLDATE OCTOBER 27, 1971LOCATION WFL 6000 INT

OPERATORS _____

TEST 3

ANALYST _____

MOISTURE DATA

	FINAL WEIGHT (gm.)	TARE WEIGHT (gm.)	WEIGHT OF MOISTURE (gm.)
IMPINGER # 1	570.4	548.8	21.6
IMPINGER # 2	582.3	575.9	6.4
IMPINGER # 3	446.3	445.4	0.9
IMPINGER # 4	662.2	651.8	10.4
	TOTAL		39.3
	MOISTURE VOLUME		39.3 ml.

PARTICULATE DATA

	FINAL WEIGHT (gm.)	TARE WEIGHT (gm.)	WEIGHT OF PARTICULATE (gm.)
FILTER	0.7393	0.7392	0.0001
BEAKER WITH (PROBE - NOZZLE - CYCLONE) WASHINGS	48.2724	48.2672	0.0052
CYCLONE FLASK	47.3040	47.2985	0.0055
BEAKER WITH (IMPINGER FILTER-HOLDER) CONTENTS AND WASHINGS	48.5269	48.5273	0.0000
	TOTAL (gm.)		0.0108
	PARTICULATES IN (mg.)		10.8

PLANT *in* Garden Oxford

BAROMETRIC PRESSURE (IN. Hg.) 29.53

STACK PRESSURE (IN. H₂O)

LOCATION WILLOW, ONTARIO

MOISTURE CONTENT VOL. %

TEST

NOZZLE DIA. IN. 0.750

DATE October 27, 1979

PROBE LENGTH $4'$ - EFFECTIVE

AMBIENT TEMPERATURE °F. 44

OPERATORS *AWG, DS, CSP*

TEST TRAVERSES

[illegible]

PARTICULATE SAMPLING DATA

STACK PRESSURE (IN. H₂O) _____

MOISTURE CONTENT VOL. %

NOZZLE DIA. IN. 0.250

PROBE LENGTH

OPERATORS

TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	88				2027.81	245	250	47	140	55	—
DB-1	2.5	88	0.54	34.02	0.44	2029.49	250	250	47	140	55	5.0
2	5.0	88	0.53	33.70	0.43	2031.14	255	250	47	160	57	5.0
3	7.5	88	0.53	33.70	0.43	2032.74	260	250	47	160	57	5.0
4	10.0	88	0.52	33.38	0.42	2034.32	260	247	46	170	55	5.0
5	12.5	88	0.525	33.54	0.42	2035.96	257	247	46	170	57	5.0
6	15.0	88	0.45	31.05	0.34	2037.46	255	247	46	170	59	4.0
	0	88	0.01			2038.03	240	220	45	105	57	—
ET-1	2.5	88	0.01	4.62	0.008	2038.26	245	220	42	107	57	5.0
2	5.0	88	0.01	4.62	0.008	2038.48	250	220	40	120	57	5.0
3	7.5	88	0.01	4.62	0.008	2038.71	252	230	40	120	57	5.0
4	10.0	88	0.01	4.62	0.008	2038.94	255	230	40	120	58	5.0
5	12.5	88	0.01	4.62	0.008	2039.17	255	230	40	120	59	5.0
6	15.0	88	0.01	4.62	0.008	2039.40	255	230	40	120	59	5.0
TOTAL	AVERAGE			AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

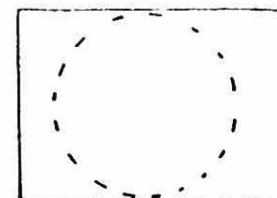
STACK PRESSURE (IN. H₂O) _____

MOISTURE CONTENT VOL. %

NOZZLE DIA. IN. 0.250

PROBE LENGTH

OPERATORS



TEST TRAVERSES

[illegible]

PARTICULATE SAMPLING DATA

STACK PRESSURE (IN. H₂O) _____

MOISTURE CONTENT VOL. %

NOZZLE DIA. IN. 0.250

PROBE LENGTH

OPERATORS



TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	96				2058.02	235	228	45	70	60	—
FT-1	2.5	96	0.01	4.66	0.001	2058.25	237	232	45	120	60	0.5
2	5.0	96	0.01	4.66	0.008	2058.49	240	242	45	130	60	0.5
3	7.5	96	0.01	4.66	0.008	2058.72	245	250	45	130	60	0.5
4	10.0	96	0.01	4.66	0.008	2058.95	248	255	45	130	60	0.5
5	12.5	96	0.01	4.66	0.008	2059.18	250	260	45	129	60	0.5
6	15.0	97	0.01	4.66	0.008	2059.42	245	255	45	130	60	0.5
	0	97				2059.42	240	270	42	120	60	
14-1	2.5	97	0.29	25.13	0.24	2060.66	240	270	44	130	61	3.0
2	5.0	97	0.25	23.33	0.19	2061.80	245	260	45	160	61	3.0
3	7.5	97	0.29	25.13	0.24	2063.04	250	260	45	165	61	3.0
4	10.0	97	0.25	23.33	0.19	2064.19	250	270	44	165	61	3.0
5	12.5	97	0.18	19.80	0.14	2065.17	250	270	45	165	61	
6	15.0	97	0.16	18.67	0.15	2066.09	250	270	42	165	61	
TOTAL	AVERAGE			AV.		TOTAL			AVERAGE		AV.	

PLANT _____

BAROMETRIC PRESSURE (IN. Hg.) 29.55STACK PRESSURE (IN. H₂O) _____

LOCATION _____

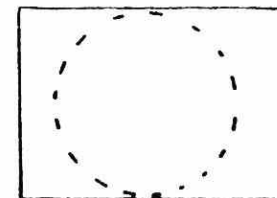
MOISTURE CONTENT VOL. % _____

TEST 4NOZZLE DIA. IN. 0.250DATE October 27, 1979

PROBE LENGTH _____

AMBIENT TEMPERATURE °F. _____

OPERATORS _____



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	97				2066.09	245	270	42	165	61	—
10-1	2.5	97	0.41	29.88	0.33	2067.55	240	280	42	165	61	3.5
2	5.0	97	0.44	30.96	0.35	2069.08	235	280	41	180	62	4.1
3	7.5	97	0.55	34.61	0.45	2070.79	235	275	41	175	62	3.5
4	10.0	97	0.51	33.33	0.41	2072.44	240	270	41	175	62	4.1
5	12.5	97	0.48	32.33	0.39	2074.06	245	270	41	175	63	4.1
6	15.0	97	0.48	32.33	0.39	2075.68	250	270	40	177	65	4.2
TOTAL		AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

Absolute stack gas pressure in in. Hg. is

$$P_s = P_{bar} + \frac{P_{static} \text{ in. H}_2\text{O}}{13.6 \text{ in. H}_2\text{O/in. Hg.}}$$

$$P_s = \frac{29.53}{13.6} + \frac{0.04}{13.6}$$

$$P_s = \underline{29.53} \text{ in. Hg.}$$

The molecular weight of the stack gas on a dry basis in lb/lb.mole. is

$$M_d = 0.44 (\% \text{ CO}_2) \text{ avg.} + 0.32 (\% \text{ O}_2) \text{ avg.} + 0.28 [(\% \text{ N}_2) \text{ avg.} + (\% \text{ CO}) \text{ avg.}]$$

$$M_d = 0.44 \times \underline{0.4} + 0.32 \times \underline{20.75} + 0.28 (\underline{77.95} + \underline{\quad})$$

$$M_d = \underline{0.176} + \underline{6.64} + \underline{21.83} + 0.36 \underline{+(0.4)(0.7)}$$

$$M_d = \underline{29.01} \text{ lb/lb.mole.}$$

The volume of water vapour collected at reference conditions in ft^3 is

$$V_{wc} = 0.0474 \text{ ft}^3/\text{ml} \times \text{volume of moisture collected ml.}$$

$$V_{wc} = 0.0474 \times \underline{67.7}$$

$$V_{wc} = \underline{3.21} \text{ ft}^3$$

The average ΔP orifice in in. H_2O is

$$\Delta P \text{ orifice avg.} = \frac{\Sigma \Delta P \text{ orifice}}{\# \text{ points}}$$

$$\Delta P \text{ orifice avg.} = \frac{\underline{11.584}}{\underline{54}}$$

$$\Delta P \text{ orifice avg.} = \underline{0.214} \text{ in. H}_2\text{O}$$

The pressure at the gas meter in in. Hg. is

$$P_m = P_{\text{bar}} + \frac{\Delta P \text{ orifice avg. in. H}_2\text{O}}{13.6 \text{ in. H}_2\text{O/in. Hg.}}$$

$$P_m = \underline{29.53} + \frac{\underline{0.214}}{\underline{13.6}}$$

$$P_m = \underline{29.53} + \underline{0.0157}$$

$$P_m = \underline{29.55} \text{ in. Hg.}$$

The temperature of the total gas meter in $^{\circ}\text{R}$. is

$$T_m = \frac{\Sigma \text{ meter temp. } ^{\circ}\text{F.}}{\# \text{ points}} + 460$$

$$T_m = \underline{\hspace{2cm}} + 460$$

$$T_m = \underline{530^{\circ}\text{R}} \quad (\text{TEMPERATURE CORRECTED})$$

The total volume of gas metered in ft^3 is

$$V_m = V_f - V_i$$

$$V_m = \underline{\hspace{2cm}} - \underline{\hspace{2cm}}$$

$$V_m = \underline{54.79} \text{ ft}^3$$

The dry gas volume at reference conditions in ft^3 is

$$V_{mc} = 17.71 \frac{^{\circ}\text{R}}{\text{in. Hg.}} \frac{V_m \text{ ft}^3 \times P_m \text{ in. Hg.}}{T_m ^{\circ}\text{R}}$$

$$V_{mc} = 17.71 \times \frac{54.79 \times 29.55}{530}$$

$$V_{mc} = \underline{54.10} \text{ ft}^3$$

The stack gas moisture content, i.e. the proportion by volume of water vapour in the gas stream is

$$B_{wo} = \frac{V_{wc} \text{ ft}^3}{V_{wc} \text{ ft}^3 + V_{mo} \text{ ft}^3} \quad (\text{using dry-basis})$$

$$B_{wo} = \frac{3.21}{3.21 + 54.10}$$

$$B_{wo} = \frac{3.21}{57.31}$$

$$B_{wo} = \underline{0.056}$$

The molecular weight of the stack gas on a wet basis in lb/lb mole. is

$$M_s = M_d \text{ lb/lb mole} (1 - B_{wo}) + 18 \text{ lb/lb mole} \times B_{wo}$$

$$M_s = \underline{29.01} \times (1 - \underline{0.056}) + 18 \times \underline{0.056}$$

$$M_s = \underline{29.01} \times \underline{0.944} + \underline{1.008}$$

$$M_s = \underline{27.385} + \underline{1.008}$$

$$M_s = \underline{28.39} \text{ lb/lb mole.}$$

The average velocity of the stack in ft./sec is

$$U_s = \frac{\sum V}{\# \text{ points}}$$

$$U_s = \frac{1118.66}{54}$$

$$U_s = \underline{20.72} \text{ ft/sec}$$

The average temperature of the stack in °R. is

$$T_s \text{ avg.} = \frac{\sum T_s}{\# \text{ points}} + 460$$

$$T_s \text{ avg.} = \frac{4973}{54} + 460$$

$$T_s \text{ avg.} = \underline{92.1} + 460$$

$$T_s \text{ avg.} = \underline{552.1}^{\circ}\text{R.}$$

The cross-sectional area of the stack in ft^2 is

$$A_s = \frac{\pi D^2}{4}$$

$$A_s = \frac{\pi}{4} \times (\text{_____})^2$$

$$A_s = 0.7854 \times \text{_____}$$

$$A_s = \underline{9.0} \text{ ft}^2 / \text{FILTER DRUM}$$

The volumetric stack gas flowrate on a dry basis at reference conditions in ft^3/hr is

$$Q_s = 3600 \text{ sec/hr} \times U_s \text{ ft/sec} \times A_s \text{ ft}^2 \times (1 - B_{wO}) \times \frac{T_{\text{ref}}}{T_{s \text{ avg.}}} \times \frac{P_s}{P_{\text{ref}}}$$

$$Q_s = 3600 \times \underline{20.72} \text{ ft/sec} \times \underline{9.0} \text{ ft}^2 \times (1 - \underline{0.056}) \times \frac{\underline{530}}{552.1 \text{ } ^\circ\text{R}} \times \frac{\underline{29.53 \text{ in. Hg.}}}{29.92 \text{ in. Hg.}}$$

$$Q_s = 3600 \times \underline{20.72} \times \underline{9.0} \times \underline{0.944} \times \underline{0.960} \times \underline{0.987}$$

$$Q_s = \underline{6.00 \times 10^5} \text{ ft}^3/\text{hr} / \text{FILTER DRUM}$$

$$\underline{1.80 \times 10^5} \text{ ft}^3/\text{hr} \text{ TOTAL}$$

The total amount of particulate matter collected in mg. is

$$M_p = \underline{14.3} \text{ mg.}$$

The concentration of particulate matter in stack gas on a dry basis at reference conditions in lb/ft^3 is

$$C_p = 2.205 \times 10^{-6} \text{ lb/mg} \times \frac{M_p}{V_{mc}}$$

$$C_p = 2.205 \times 10^{-6} \times \frac{14.3 \text{ mg}}{54.10 \text{ ft}^3}$$

$$C_p = \underline{5.81 \times 10^{-7}} \text{ lb/ft}^3$$

The emission rate of particulate matter from the stack on a dry basis at reference conditions in lb/hr is

$$E_{rp} = C_p \text{ lb/ft}^3 \times Q_s \text{ ft}^3/\text{hr}$$

$$E_{rp} = \underline{5.81 \times 10^{-7}} \times \underline{6.00 \times 10^5}$$

$$E_{rp} = \underline{0.349} \text{ lb/hr} / \text{FILTER CRUM}$$
$$\underline{1.05} \text{ lb/hr}$$

PLANT GRAND DRIER
 LOCATION NEWBURY ONT
 TEST 4

DATE OCTOBER 27 1929
 OPERATORS _____
 ANALYST _____

MOISTURE DATA

	FINAL WEIGHT (gm.)	TARE WEIGHT (gm.)	WEIGHT OF MOISTURE (gm.)
IMPINGER # 1	618.6	576.1	42.5
IMPINGER # 2	595.3	583.8	11.5
IMPINGER # 3	449.8	446.7	3.1
IMPINGER # 4	674.3	663.7	10.6
TOTAL			67.7
MOISTURE VOLUME			67.7 ml.

PARTICULATE DATA

	FINAL WEIGHT (gm.)	TARE WEIGHT (gm.)	WEIGHT OF PARTICULATE (gm.)
FILTER	0.7567	0.7561	0.0006
BEAKER WITH (PROBE - NOZZLE - CYCLONE) WASHINGS	48.7295	48.7261	0.0034
CYCLONE FLASK	47.7174	47.7072	0.0102
BEAKER WITH (IMPINGER FILTER-HOLDER) CONTENTS AND WASHINGS	46.7007	46.7006	0.0001
TOTAL (gm.)			0.0143
PARTICULATES IN (mg.)			14.3

MODEL 2165-D
PLANT ACE GRAIN DRYER

BAROMETRIC PRESSURE (IN. Hg.) 29.57

STACK PRESSURE (IN. H₂O) _____

LOCATION NEW BURY, ONTARIO

MOISTURE CONTENT VOL. % _____

TEST 5

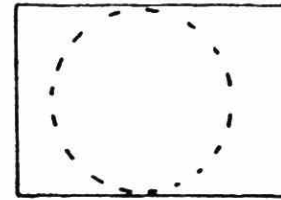
NOZZLE DIA. IN. 0.25

DATE Nov. 2 / 79

PROBE LENGTH 4' EFFECTIVE

AMBIENT TEMPERATURE °F. 45

OPERATORS D.S., C.S.T.P., A.W.G.



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. IN. Hg.
									OUTLET	INLET		
	0	89				2109.03	260	170	88	151	40	0.5'
A-1	2.5'	89	0.03	8.00	0.024	2109.44	260	170	88	151	40	0.5'
2	5.0	89	0.02	6.53	0.016	2109.76	260	195	80	210	40	0.5'
3	7.5	89	0.01	4.62	0.008	2109.99	260	215	80	230	40	0.5'
4	10.0	89	0.01	4.62	0.008	2110.21	255	240	82	242	40	0.5'
5	12.5	89	0.01	4.62	0.008	2110.45	250	255	85	250	40	0.5'
6	15.0	89	0.01	4.62	0.008	2110.68	245	270	88	262	42	0.5'
	0	89				2111.02	245	280	80	240	45	3.0
B-1	2.5'	89	0.28	24.45	0.224	2112.28	245	280	80	240	45	3.0
2	5.0	89	0.28	24.45	0.224	2113.53	240	260	75	230	44	3.0
3	7.5	93	0.27	24.10	0.22	2114.76	240	272	74	235	45	3.2
4	10.0	93	0.22	21.75	0.176	2115.85	245	272	73	240	45	2.7
5	12.5	93	0.26	23.65	0.21	2117.03	240	275	79	240	50	3.2
6	15.0	93	0.19	20.21	0.15	2118.05	235	280	79	241	50	2.5
TOTAL	AVERAGE			AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

PLANT _____

BAROMETRIC PRESSURE (IN. Hg.) _____

STACK PRESSURE (IN. H₂O) _____

LOCATION _____

MOISTURE CONTENT VOL. % _____

TEST 5 _____

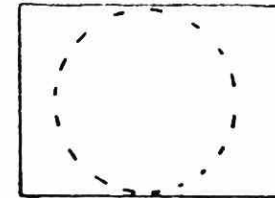
NOZZLE DIA. IN. _____

DATE Nov. 2/79 _____

PROBE LENGTH _____

AMBIENT TEMPERATURE °F. _____

OPERATORS _____



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0					2118.49	240	280	85	240	51	4.2
AB-1	2.5	93	0.45	31.11	0.36	2120.07	245	280	85	240	51	4.2
2	5.0	93	0.52	33.43	0.42	2121.71	250	270	79	240	52	4.2
3	7.5	93	0.49	32.46	0.45	2123.29	255	265	78	240	52	4.1
4	10.0	93	0.46	31.45	0.37	2124.89	250	270	80	240	55	4.2
5	12.5	93	0.40	29.33	0.32	2126.39	250	270	80	230	56	4.1
6	15.0	93	0.39	28.96	0.31	2127.87	250	270	82	240	60	4.0
TOTAL		AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

PLANT _____

BAROMETRIC PRESSURE (IN. Hg.) _____

STACK PRESSURE (IN. H₂O) _____

LOCATION _____

MOISTURE CONTENT VOL. % _____

TEST 5

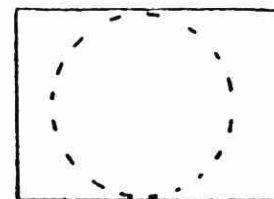
NOZZLE DIA. IN. _____

DATE NOV. 2/79

PROBE LENGTH _____

AMBIENT TEMPERATURE °F. _____

OPERATORS _____



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	94				2128.00	235	240	100	121	60	0.5
BT-1	2.5	94	0.01	4.64	0.008	2128.23	235	240	100	121	60	0.5
2	5.0	94	0.01	4.64	0.008	2128.46	240	235	89	200	60	0.5
3	7.5	94	0.01	4.64	0.008	2128.68	240	240	80	207	60	0.5
4	10.0	94	0.01	4.64	0.008	2128.91	240	250	81	225	61	0.5
5	12.5	94	0.01	4.64	0.008	2129.15	240	255	80	235	60	0.5
6	15.0	94	0.01	4.64	0.008	2129.38	245	270	80	240	62	0.5
	0	96				2129.51	245	280	80	240	61	4.7
BT-1	2.5	96	0.38	28.66	0.31	2130.93	250	280	80	240	61	4.7
2	5.0	96	0.30	25.47	0.25	2132.01	260	290	72	257	61	4.5
3	7.5	96	0.28	24.60	0.23	2133.08	265	290	72	260	61	4.4
4	10.0	96	0.28	24.60	0.23	2134.25	265	290	78	260	65	4.4
5	12.5	96	0.21	21.31	0.17	2135.34	265	285	78	260	64	3.8
6	15.0	96	0.21	21.31	0.17	2136.43	260	285	75	250	65	3.8
	TOTAL	AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

PLANT _____

BAROMETRIC PRESSURE (IN. Hg.) _____

STACK PRESSURE (IN. H₂O) _____

LOCATION _____

MOISTURE CONTENT VOL. % _____

TEST 5

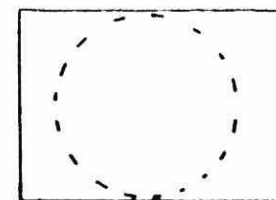
NOZZLE DIA. IN. _____

DATE NOV. 2/79

PROBE LENGTH _____

AMBIENT TEMPERATURE °F. _____

OPERATORS _____



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	96				2137.03	260	285	75	242	65	6.0
BB-1	2.5	96	0.53	34.48	0.45	2138.72	255	285	75	242	65	6.0
2	5.0	96	0.52	33.53	0.43	2140.41	250	285	73	255	65	6.0
3	7.5	96	0.50	32.88	0.42	2142.06	255	282	78	245	65	6.0
4	10.0	97	0.52	33.56	0.43	2143.73	255	275	80	260	66	6.2
5	12.5	97	0.50	32.91	0.42	2145.38	250	275	75	250	67	6.1
6	15.0	97	0.40	29.43	0.33	2146.88	245	280	75	250	67	5.2
TOTAL		AVERAGE		AV.	TOTAL			AVERAGE		AV.		

PARTICULATE SAMPLING DATA

F-31

PLANT _____

BAROMETRIC PRESSURE (IN. Hg.) _____

STACK PRESSURE (IN. H₂O) _____

LOCATION _____

MOISTURE CONTENT VOL. % _____

TEST 5'

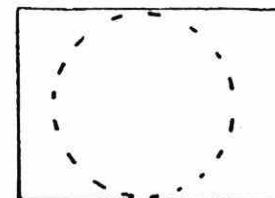
NOZZLE DIA. IN. _____

DATE NOV. 2/79

PROBE LENGTH _____

AMBIENT TEMPERATURE °F. _____

OPERATORS _____



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	100				2147.04	240	230	85	140	65	0.5
CT-1	2.5	100	0.01	4.23	0.008	2147.25	253	230	85	140	65	0.5
2	5.0	100	0.01	4.23	0.008	2147.45	270	237	85	175	62	0.5
3	7.5	100	0.01	4.23	0.008	2147.65	280	235	77	190	60	0.5
4	10.0	100	0.01	4.23	0.008	2147.86	270	250	80	210	60	0.5
5'	12.5	100	0.01	4.23	0.008	2148.07	275	272	85	230	60	0.5
6	15.0	100	0.01	4.23	0.008	2148.28	275	295	88	250	60	0.5
	0	100				2148.46	265	300	88	250	60	3.0
CH-1	2.5	100	0.24	20.72	0.20	2149.48	265	300	88	250	60	3.0
2	5.0	100	0.26	21.57	0.22	2150.53	270	295	80	245	62	3.0
3	7.5	100	0.24	20.72	0.20	2151.55	265	285	80	240	62	3.0
4	10.0	100	0.17	17.44	0.14	2152.40	260	280	80	235	62	2.2
5'	12.5	100	0.3	23.16	0.25	2153.54	260	270	80	230	62	3.2
6	15.0	100	0.25	21.15	0.21	2154.60	255	265	80	230	60	3.0
	TOTAL	AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

PLANT _____

BAROMETRIC PRESSURE (IN. Hg.) _____

STACK PRESSURE (IN. H₂O) _____

LOCATION _____

MOISTURE CONTENT VOL. % _____

TEST 3

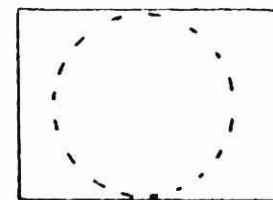
NOZZLE DIA. IN. _____

DATE Nov. 2/79

PROBE LENGTH _____

AMBIENT TEMPERATURE °F. _____

OPERATORS _____



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	100				215'4.77	240	260	90	195	60	4.5
CB-1	2.5	100	0.55	31.37	0.45	215'6.32	245	260	90	195	60	4.5
2	5.0	100	0.51	30.20	0.41	215'7.80	240	250	87	230	60	4.5
3	7.5	100	0.48	29.30	0.39	215'9.24	240	255	86	235	60	4.5
4	10.0	100	0.3	23.16	0.25	2160.39	235	260	90	242	60	3.3
5	12.5	100	0.52	30.50	0.42	2161.92	235	270	88	242	62	4.5
6	15.0	100	0.4	26.75	0.33	2163.24	230	275	88	245	62	3.8
TOTAL		AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

Absolute stack gas pressure in in. Hg. is

$$P_s = P_{bar} + \frac{P_{static} \text{ in. H}_2\text{O}}{13.6 \text{ in. H}_2\text{O/in. Hg.}}$$

$$P_s = \underline{29.57} + \frac{0.04}{13.6}$$

$$P_s = \underline{29.57} \text{ in. Hg.}$$

The molecular weight of the stack gas on a dry basis in lb/lb.mole. is

$$M_d = 0.44 (\% \text{ CO}_2) \text{ avg.} + 0.32 (\% \text{ O}_2) \text{ avg.} + 0.28 [(\% \text{ N}_2) \text{ avg.} + (\% \text{ CO}) \text{ avg.}]$$

$$M_d = 0.44 \times \underline{0.4} + 0.32 \times \underline{20.75} + 0.28 (\underline{77.95} + \underline{\quad})$$

$+ 0.4 \times 0.9$

$$M_d = \underline{0.176} + \underline{6.64} + \underline{21.826} + 0.36$$

$$M_d = \underline{29.002} \text{ lb/lb mole.}$$

The volume of water vapour collected at reference conditions in ft^3 is

$$V_{wo} = 0.0474 \text{ ft}^3/\text{ml} \times \text{volume of moisture collected ml.}$$

$$V_{wc} = 0.0474 \times \underline{50.8}$$

$$V_{wc} = \underline{2.408} \text{ ft}^3$$

The average ΔP orifice in in. H_2O is

$$\Delta P \text{ orifice avg.} = \frac{\Sigma \Delta P \text{ orifice}}{\# \text{ points}}$$

$$\Delta P \text{ orifice avg.} = \frac{\underline{10.912}}{\underline{54}}$$

$$\Delta P \text{ orifice avg.} = \underline{0.202} \text{ in. H}_2\text{O}$$

The pressure at the gas meter in in. Hg. is

$$P_m = P_{\text{bar}} + \frac{\Delta P \text{ orifice avg. in. H}_2\text{O}}{13.6 \text{ in. H}_2\text{O/in. Hg.}}$$

$$P_m = \underline{29.57} + \frac{\underline{0.202}}{\underline{13.6}}$$

$$P_m = \underline{29.57} + \underline{0.015}$$

$$P_m = \underline{29.59} \text{ in. Hg.}$$

The temperature of the total gas meter in $^{\circ}\text{R}$. is

$$T_m = \frac{\text{I meter temp. } ^{\circ}\text{F.}}{\# \text{ points}} + 460$$

$$T_m = \frac{70}{\quad} + 460$$

$$T_m = \underline{530^{\circ}\text{R}} \quad \text{Temperature Compensated}$$

The total volume of gas metered in ft^3 is

$$V_m = V_f - V_i$$

$$V_m = \underline{\quad} - \underline{\quad}$$

$$V_m = \underline{52.06} \text{ ft}^3$$

The dry gas volume at reference conditions in ft^3 is

$$V_{mc} = 17.71 \frac{^{\circ}\text{R}}{\text{in. Hg.}} \frac{V_m \text{ ft}^3 \times P_m \text{ in. Hg.}}{T_m ^{\circ}\text{R}}$$

$$V_{mc} = 17.71 \times \frac{52.06 \times 29.59}{530}$$

$$V_{mc} = \underline{51.474} \text{ ft}^3$$

The stack gas moisture content, i.e. the proportion by volume of water vapour in the gas stream is

$$B_{wo} = \frac{V_{wc} \text{ ft}^3}{V_{wc} \text{ ft}^3 + V_{mo} \text{ ft}^3} \quad (\text{using dry-basis})$$

$$B_{wo} = \frac{2.408}{2.408 + 51.474}$$

$$B_{wo} = \frac{2.408}{53.882}$$

$$B_{wo} = \underline{0.0447}$$

The molecular weight of the stack gas on a wet basis in lb/lb mole. is

$$M_s = M_d \text{ lb/lb mole } (1 - B_{wo}) + 18 \text{ lb/lb mole } \times B_{wo}$$

$$M_s = \underline{29.002} \times (1 - \underline{0.0447}) + 18 \times \underline{0.0447}$$

$$M_s = \underline{29.002} \times \underline{0.9553} + \underline{0.8046}$$

$$M_s = \underline{27.706} + \underline{0.8046}$$

$$M_s = \underline{28.511} \text{ lb/lb mole.}$$

The average velocity of the stack in ft/sec is

$$U_s = \frac{\sum V}{\# \text{ points}}$$

$$U_s = \frac{1050.36}{54}$$

$$U_s = \underline{19.45} \text{ ft/sec}$$

The average temperature of the stack in °R. is

$$T_s \text{ avg.} = \frac{\sum T_s}{\# \text{ points}} + 460$$

$$T_s \text{ avg.} = \frac{5925}{63} + 460$$

$$T_s \text{ avg.} = \underline{94.05} + 460$$

$$T_s \text{ avg.} = \underline{554.05} \text{ °R.}$$

The cross-sectional area of the stack in ft^2 is

$$A_s = \frac{\pi D^2}{4}$$

$$A_s = \frac{\pi}{4} \times (\text{_____})^2$$

$$A_s = 0.7854 \times \text{_____}$$

$$A_s = \underline{9} \text{ ft}^2 / \text{FILTER DRUM}$$

The volumetric stack gas flowrate on a dry basis at reference conditions in ft^3/hr is

$$Q_s = 3600 \text{ sec/hr} \times U_s \text{ ft/sec} \times A_s \text{ ft}^2 \times (1 - B_{wO}) \\ \times \frac{T_{\text{ref}}}{T_{s \text{ avg.}}} \times \frac{P_s}{P_{\text{ref}}}$$

$$Q_s = 3600 \times \underline{19.45} \text{ ft/sec} \times \underline{9} \text{ ft}^2 \times (1 - \underline{0.0447}) \\ \times \frac{530}{534.05^\circ\text{R}} \times \frac{29.57 \text{ in. Hg.}}{29.92 \text{ in. Hg.}}$$

$$Q_s = 3600 \times \underline{19.45} \times \underline{9} \times \underline{0.9553} \times \underline{0.9566} \times \underline{0.9883}$$

$$Q_s = \underline{5.691 \times 10^5} \text{ ft}^3/\text{hr} / \text{FILTER DRUM}$$

The total amount of particulate matter collected in mg. is

$$M_p = \underline{15.0} \text{ mg.}$$

The concentration of particulate matter in stack gas on a dry basis at reference conditions in lb/ft^3 is

$$C_p = 2.205 \times 10^{-6} \text{ lb/mg} \times \frac{M_p}{V_{mc}}$$

$$C_p = 2.205 \times 10^{-6} \times \frac{15.0 \text{ mg}}{51.474 \text{ ft}^3}$$

$$C_p = \underline{6.426 \times 10^{-7}} \text{ lb/ft}^3$$

The emission rate of particulate matter from the stack on a dry basis at reference conditions in lb/hr is

$$E_{rp} = C_p \text{ lb/ft}^3 \times Q_s \text{ ft}^3/\text{hr}$$

$$E_{rp} = \underline{6.426 \times 10^{-7}} \times \underline{5.691 \times 10^5}$$

$$E_{rp} = \underline{0.366} \text{ lb/hr} / \text{FILTER DRUM}$$

$$= \underline{1.098 \text{ lb/hr Total}}$$

PLANT SAND OILERDATE NOVEMBER 1959LOCATION NEWBURY DATA

OPERATORS _____

TEST 5

ANALYST _____

MOISTURE DATA

	FINAL WEIGHT (gm.)	TARE WEIGHT (gm.)	WEIGHT OF MOISTURE (gm.)
IMPINGER # 1	5847	557.5	27.2
IMPINGER # 2	572.4	562.9	9.5
IMPINGER # 3	4413	439.5	1.8
IMPINGER # 4	671.5	659.2	12.3
TOTAL			50.8
MOISTURE VOLUME			50.8 ml.

PARTICULATE DATA

	FINAL WEIGHT (gm.)	TARE WEIGHT (gm.)	WEIGHT OF PARTICULATE (gm.)
FILTER	0.7556	0.7551	0.0005
BEAKER WITH (PROBE - NOZZLE - CYCLONE) WASHINGS	51.0589	51.0542	0.0047
CYCLONE FLASK	48.7645	48.7552	0.0093
BEAKER WITH (IMPINGER FILTER-HOLDER) CONTENTS AND WASHINGS	48.8082	48.8077	0.0005
TOTAL (gm.)			0.0150
PARTICULATES IN (mg.)			15.0

STACK PRESSURE (IN. H₂O)

MOISTURE CONTENT VOL. %

NOZZLE DIA. IN. 0.250

PROBE LENGTH λ' EFFECTIVE

OPERATORS *AWG, DS, CSP*

TEST TRAVERSES

1
2
3

PARTICULATE SAMPLING DATA

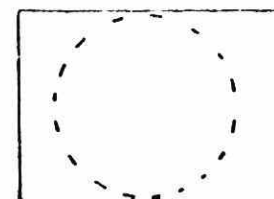
STACK PRESSURE (IN. H₂O)

MOISTURE CONTENT VOL. %

NOZZLE DIA. IN. 0.250

PROBE LENGTH

OPERATORS



TEST TRAVERSES

[illegible]

PARTICULATE SAMPLING DATA

STACK PRESSURE (IN. H₂O) _____

MOISTURE CONTENT VOL. %

NOZZLE DIA. IN. 0.250

PROBE LENGTH _____

OPERATORS

TEST TRAVERSES

1-4
1-4
1

PARTICULATE SAMPLING DATA

PLANT _____

BAROMETRIC PRESSURE (IN. Hg.) _____

STACK PRESSURE (IN. H₂O) _____

LOCATION _____

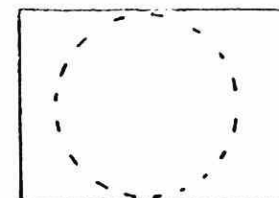
MOISTURE CONTENT VOL. % _____

TEST 6NOZZLE DIA. IN. 0.250DATE November 2, 1979

PROBE LENGTH _____

AMBIENT TEMPERATURE °F. _____

OPERATORS _____



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	100				2210.02	235	240	44	115	60	—
FT-1	2.5	100	0.01	4.68	0.008	2210.25	235	252	41	115	60	0.0
2	5.0	102	0.01	4.69	0.008	2210.48	240	255	48	125	60	0.0
3	7.5	102	0.01	4.69	0.008	2210.70	240	257	48	140	60	0.0
4	10.0	102	0.01	4.69	0.008	2210.93	242	260	48	147	60	0.0
5	12.5	102	0.01	4.69	0.008	2211.16	245	265	49	157	60	0.0
6	15.0	102	0.01	4.69	0.008	2211.38	248	275	41	165	61	0.0
	0	102				2211.38	235	275	41	165	61	—
FM-1	2.5	102	0.30	15.68	0.25	2212.62	240	277	44	165	61	4.0
2	5.0	102	0.24	17.97	0.20	2213.73	245	280	45	200	62	3.4
3	7.5	102	0.21	21.98	0.17	2214.78	250	290	45	200	62	3.0
4	10.0	102	0.16	18.75	0.13	2215.66	250	290	45	200	62	2.0
5	12.5	102	0.21	21.48	0.17	2216.68	250	290	48	202	65	3.2
6	15.0	102	0.19	19.45	0.15	2217.65	250	290	48	205	65	3.0
	TOTAL	AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

PLANT _____

BAROMETRIC PRESSURE (IN. Hg.) _____

STACK PRESSURE (IN. H₂O) _____

LOCATION _____

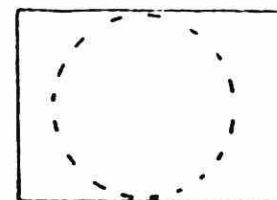
MOISTURE CONTENT VOL. % _____

TEST 6NOZZLE DIA. IN. 0.250DATE November 2, 1979

PROBE LENGTH _____

AMBIENT TEMPERATURE °F. _____

OPERATORS _____



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	102				2217.65	245	285	48	200	65	—
F0-1	2.5	102	0.38	28.90	0.31	2219.04	240	290	48	200	65	1
2	5.0	102	0.34	27.34	0.27	2220.36	240	290	48	200	65	1.2
3	7.5	102	0.43	30.74	0.35	2221.83	235	295	48	210	64	2.2
4	10.0	102	0.39	29.28	0.32	2223.24	235	295	48	210	60	3.0
5	12.5	102	0.41	30.02	0.34	2224.68	235	300	50	210	55	3.0
6	15.0	102	0.38	28.90	0.33	2226.08	235	300	50	210	55	3.0
	TOTAL	AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

Absolute stack gas pressure in in. Hg. is

$$P_s = P_{bar} + \frac{P_{static} \text{ in. H}_2\text{O}}{13.6 \text{ in. H}_2\text{O/in. Hg.}}$$

$$P_s = \underline{29.57} + \frac{0.04}{13.6}$$

$$P_s = \underline{29.57} \text{ in. Hg.}$$

The molecular weight of the stack gas on a dry basis in lb/lb.mole. is

$$M_d = 0.44 (\% \text{ CO}_2) \text{ avg.} + 0.32 (\% \text{ O}_2) \text{ avg.} + 0.28 [(\% \text{ N}_2) \text{ avg.} + (\% \text{ CO}) \text{ avg.}]$$

$$M_d = 0.44 \times \underline{0.40} + 0.32 \times \underline{20.8} + 0.28 (\underline{77.9} + \underline{\quad})$$

$$M_d = \underline{0.176} + \underline{6.656} + \underline{21.812} + 0.40(0.9)$$

$$M_d = \underline{29.00} \text{ lb/lb.mole.} + 0.36$$

The volume of water vapour collected at reference conditions in ft^3 is

$$V_{wc} = 0.0474 \text{ ft}^3/\text{ml} \times \text{volume of moisture collected ml.}$$

$$V_{wc} = 0.0474 \times \underline{61.2}$$

$$V_{wc} = \underline{2.90} \text{ ft}^3$$

The average ΔP orifice in in. H_2O is

$$\Delta P \text{ orifice avg.} = \frac{\Sigma \Delta P \text{ orifice}}{\# \text{ points}}$$

$$\Delta P \text{ orifice avg.} = \frac{\underline{7.492}}{\underline{54}}$$

$$\Delta P \text{ orifice avg.} = \underline{0.157} \text{ in. H}_2\text{O}$$

The pressure at the gas meter in in. Hg. is

$$P_m = P_{\text{bar}} + \frac{\Delta P \text{ orifice avg. in. H}_2\text{O}}{13.6 \text{ in. H}_2\text{O/in. Hg.}}$$

$$P_m = \underline{29.57} + \frac{\underline{0.157}}{\underline{13.6}}$$

$$P_m = \underline{29.57} + \underline{0.012}$$

$$P_m = \underline{29.58} \text{ in. Hg.}$$

The temperature of the total gas meter in $^{\circ}\text{R}$. is

$$T_m = \frac{\text{L meter temp. } ^{\circ}\text{F.}}{\text{\# points}} + 460$$

$$T_m = \underline{\hspace{2cm}} + 460$$

$$T_m = \underline{530^{\circ}\text{R}} \quad (\text{TEMPERATURE CORRECTION})$$

The total volume of gas metered in ft^3 is

$$V_m = V_f - V_i$$

$$V_m = \underline{\hspace{2cm}} - \underline{\hspace{2cm}}$$

$$V_m = \underline{46.74} \text{ ft}^3$$

The dry gas volume at reference conditions in ft^3 is

$$V_{mc} = 17.71 \frac{^{\circ}\text{R}}{\text{in. Hg.}} \quad \frac{V_m \text{ ft}^3 \times P_m \text{ in. Hg.}}{T_m ^{\circ}\text{R}}$$

$$V_{mc} = 17.71 \times \frac{46.74 \times 29.58}{530}$$

$$V_{mc} = \underline{46.20} \text{ ft}^3$$

The stack gas moisture content, i.e. the proportion by volume of water vapour in the gas stream is

$$B_{wo} = \frac{V_{wc} \text{ ft}^3}{V_{wc} \text{ ft}^3 + V_{mc} \text{ ft}^3} \quad (\text{using dry-basis})$$

$$B_{wo} = \frac{2.90}{2.90 + 46.20}$$

$$B_{wo} = \underline{0.059}$$

$$B_{wo} = \underline{0.059}$$

The molecular weight of the stack gas on a wet basis in lb/lb mole. is

$$M_s = M_d \text{ lb/lb mole} (1 - B_{wo}) + 18 \text{ lb/lb mole} \times B_{wo}$$

$$M_s = \underline{29.00} \times (1 - \underline{0.059}) + 18 \times \underline{0.059}$$

$$M_s = \underline{29.00} \times \underline{0.941} + \underline{1.062}$$

$$M_s = \underline{27.289} + \underline{1.062}$$

$$M_s = \underline{28.35} \text{ lb/lb mole.}$$

The average velocity of the stack in ft/sec is

$$U_s = \frac{\sum V}{\# \text{ points}}$$

$$U_s = \frac{970.33}{54}$$

$$U_s = \underline{17.97} \text{ ft/sec}$$

The average temperature of the stack in °R. is

$$T_s \text{ avg.} = \frac{\sum T_s}{\# \text{ points}} + 460$$

$$T_s \text{ avg.} = \frac{5370}{54} + 460$$

$$T_s \text{ avg.} = \underline{99.44} + 460$$

$$T_s \text{ avg.} = \underline{559.4} \text{ °R.}$$

The cross-sectional area of the stack in ft^2 is

$$A_s = \frac{\pi D^2}{4}$$

$$A_s = \frac{\pi}{4} \times (\text{_____})^2$$

$$A_s = 0.7854 \times \text{_____}$$

$$A_s = \underline{9.0} \text{ ft}^2 / \text{FILTER DRUM}$$

The volumetric stack gas flowrate on a dry basis at reference conditions in ft^3/hr is

$$Q_s = 3600 \text{ sec/hr} \times U_s \text{ ft/sec} \times A_s \text{ ft}^2 \times (1 - B_{wO})$$

$$\times \frac{T_{\text{ref}}}{T_{s \text{ avg.}}} \times \frac{P_s}{P_{\text{ref}}}$$

$$Q_s = 3600 \times \underline{17.97} \text{ ft/sec} \times \underline{9.0} \text{ ft}^2 \times (1 - \underline{0.059})$$

$$\times \frac{530}{559.4^\circ\text{R}} \times \frac{29.57 \text{ in. Hg.}}{29.92 \text{ in. Hg.}}$$

$$Q_s = 3600 \times \underline{17.97} \times \underline{9.0} \times \underline{0.941} \times \underline{0.9974} \times \underline{0.9613}$$

$$Q_s = \underline{5.13 \times 10^5} \text{ ft}^3/\text{hr} / \text{FILTER DRUM}$$

$$= \underline{1.54 \times 10^6} \text{ ft}^3/\text{hr} \text{ Total}$$

The total amount of particulate matter collected in mg. is

$$M_p = \underline{9.3} \text{ mg.}$$

The concentration of particulate matter in stack gas on a dry basis at reference conditions in lb/ft³ is

$$C_p = 2.205 \times 10^{-6} \text{ lb/mg} \times \frac{M_p}{V_{mc}}$$

$$C_p = 2.205 \times 10^{-6} \times \frac{9.3 \text{ mg}}{46.20 \text{ ft}^3}$$

$$C_p = \underline{4.44 \times 10^{-7}} \text{ lb/ft}^3$$

The emission rate of particulate matter from the stack on a dry basis at reference conditions in lb/hr is

$$ER_p = C_p \text{ lb/ft}^3 \times Q_s \text{ ft}^3/\text{hr}$$

$$ER_p = \underline{4.44 \times 10^{-7}} \times \underline{5.13 \times 10^5} / \text{FILTER DRUM}$$

$$ER_p = \underline{0.228} \text{ lb/hr} / \text{FILTER DRUM}$$

$$= \underline{0.684} \text{ lb/hr}$$

PLANT GRAIN DRYERDATE NOVEMBER 2 1929LOCATION NEWBURY, ONTARIO

OPERATORS _____

TEST 6

ANALYST _____

MOISTURE DATA

	FINAL WEIGHT (gm.)	TARE WEIGHT (gm.)	WEIGHT OF MOISTURE (gm.)
IMPINGER # 1	630.8	591.4	39.4
IMPINGER # 2	581.2	573.7	7.5
IMPINGER # 3	443.0	441.5	1.5
IMPINGER # 4	675.2	662.4	12.8
TOTAL			61.2
MOISTURE VOLUME			61.2 ml.

PARTICULATE DATA

	FINAL WEIGHT (gm.)	TARE WEIGHT (gm.)	WEIGHT OF PARTICULATE (gm.)
FILTER	0.7662	0.7663	0.0000
BEAKER WITH (PROBE - NOZZLE - CYCLONE) WASHINGS	51.0612	51.0592	0.0020
CYCLONE FLASK	46.3421	46.3352	0.0069
BEAKER WITH (IMPINGER FILTER-HOLDER) CONTENTS AND WASHINGS	48.8071	48.8067	0.0004
TOTAL (gm.)			0.0093
PARTICULATES IN (mg.)			9.3

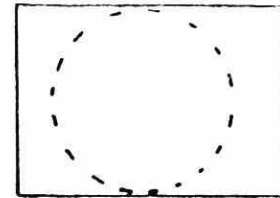
STACK PRESSURE (IN. H₂O)

MOISTURE CONTENT VOL. %

NOZZLE DIA. IN. 0.250

PROBE LENGTH 4'

OPERATORS *AVG, OS, CSP*



TEST TRAVERSES

[illegible]

PARTICULATE SAMPLING DATA

453

MODEL 21CS-D
PLANT ACE GRAIN DRYER

BAROMETRIC PRESSURE (IN. Hg.) 29.53

STACK PRESSURE (IN. H₂O) _____

LOCATION NEWBURY, ONTARIO

MOISTURE CONTENT VOL. % _____

TEST HENDERSEN TEST 2

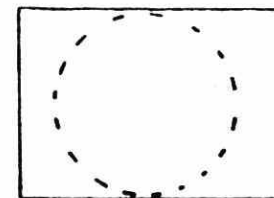
NOZZLE DIA. IN. 0.375

DATE OCT. 27/79

PROBE LENGTH 4' EFFECTIVE

AMBIENT TEMPERATURE °F. 44

OPERATORS R.W.G., D.S., C.S.T.P.



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	105				2080.01	275	270	40	180	64	9.0
FB-1	5	105	0.42	30.46	0.9	2084.75	275	270	40	180	64	9.0
2	10	105	0.53	34.22	0.9	2089.48	280	280	41	205	64	9.0
3	15	105	0.48	32.57	0.9	2094.23	280	290	41	220	62	9.0
4	20	105	0.27	24.12	0.9	2099.04	280	290	45	200	65	9.0
5	25	105	0.27	24.42	0.9	2103.88	285	270	45	215	65	9.0
6	30	105	0.17	24.12	0.9	2108.72	285	225	41	190	62	9.0
TOTAL		AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

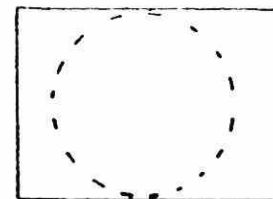
STACK PRESSURE (IN. H₂O)

MOISTURE CONTENT VOL. %

NOZZLE DIA. IN. 0.375

PROBE LENGTH 4' Effluent

OPERATORS *AWG, DS, CSP*



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	70				2230.46	230	230	46	135	53	—
M-1	5	90	0.26	21.39	0.81	2235.02	235	235	45	145	55	10.0
2	10	90	0.26	21.39	0.78	2239.50	240	240	48	185	57	10.0
3	15	95	0.18	19.77	0.76	2243.89	245	245	50	190	58	10.0
4	20	95	0.18	19.77	0.755	2248.29	240	252	55	200	60	10.0
5	25	100	0.20	20.93	0.755	2252.66	240	252	55	200	60	10.0
6	30	100	0.20	20.93	0.75	2257.05	240	251	55	200	60	10.0
	TOTAL	AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

APPENDIX III
NATURAL GAS COMPOSITION

Component	% by Volume
Methane	94 .
Ethane	2.960
Propane	0.350
Isobutane	0.030
Butane	0.040
Isopentane	0.002
Nitrogen	2.170
Carbon Dioxide	0.41

TABLE III.1: Composition of Natural Gas Supplied to the Newbury, Ontario Region [12]

APPENDIX III
NATURAL GAS COMPOSITION

These data are on file with:

Technology Development and Appraisal Section
Air Resources Branch
Ministry of the Environment
Province of Ontario
880 Bay Street, 4th Floor
Toronto, Ontario M5S 1Z8

Component	% by Volume
Methane	94
Ethane	2.960
Propane	0.350
Isobutane	0.030
Butane	0.040
Isopentane	0.002
Nitrogen	2.170
Carbon Dioxide	0.41

TABLE III.1: Composition of Natural Gas Supplied to the Newbury, Ontario Region [12]

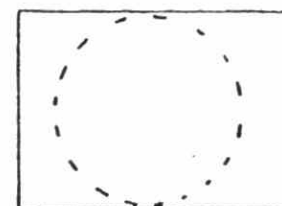
PLANT ALCO GND. 2011 BAROMETRIC PRESSURE (IN. Hg.) 29.47 STACK PRESSURE (IN. H₂O)

LOCATION NE. JURY, ONTARIO MOISTURE CONTENT VOL. %

TEST ANDERSEN 1 NOZZLE DIA. IN. 0.250

DATE OCTOBER 26, 1979 PROBE LENGTH 1'

AMBIENT TEMPERATURE °F. 42 OPERATORS AWG, DS, CSP



TEST TRAVERSES C_P = .671

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	93				1936.28	275	250	44	165	55	
1B-1	5	93	0.58	35.34	0.56	1940.92	280	255	41	165	55	6.0
2	10	93	0.58	35.34	0.56	1944.14	285	260	41	170	55	6.0
3	15	93	0.55	34.92	0.56	1947.98	270	260	41	170	55	6.0
4	20	93	0.62	36.54	0.56	1951.80	280	255	42	175	55	6.0
5	25	93	0.60	35.95	0.56	1955.63	275	260	42	175	55	6.0
6	30	93	0.52	33.46	0.56	1959.43	270	260	42	175	55	6.0
TOTAL		AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

PLANT HEE GRAIN DRYER

BAROMETRIC PRESSURE (IN. Hg.) 29.53

STACK PRESSURE (IN. H₂O) _____

LOCATION NEWBURY, ONTARIO

MOISTURE CONTENT VOL. % _____

TEST HANDERSEN TEST 2

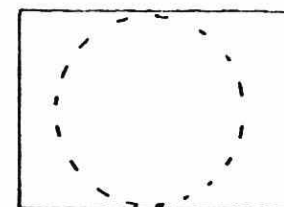
NOZZLE DIA. IN. 0.375

DATE OCT. 27/79

PROBE LENGTH 4' EFFECTIVE

AMBIENT TEMPERATURE °F 44

OPERATORS AWG, D.S., C.S.T.P.



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	105				2080.01	275	270	40	180	64	9.0
FB-1	5	105	0.42	30.46	0.9	2084.75	275	270	40	180	64	9.0
2	10	105	0.53	34.22	0.9	2089.48	280	280	41	205	64	9.0
3	15	105	0.48	32.57	0.9	2094.23	280	290	41	220	62	9.0
4	20	105	0.27	24.42	0.9	2099.04	280	290	45	200	65	9.0
5	25	105	0.27	24.42	0.9	2103.88	285	270	45	215	65	9.0
6	30	105	0.17	24.42	0.9	2108.72	285	225	41	190	62	9.0
TOTAL		AVERAGE		AV.	TOTAL			AVERAGE		AV.		

PARTICULATE SAMPLING DATA

159

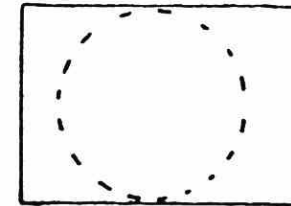
PLANT ACC. GARDEN CENTER BAROMETRIC PRESSURE (IN. Hg.) 29.57 STACK PRESSURE (IN. H₂O)

LOCATION ALFORD, DARTMOUTH MOISTURE CONTENT VOL. %

TEST ANDERSEN 3 NOZZLE DIA. IN. 0.375

DATE NOVEMBER 2, 1979 PROBE LENGTH 4' EFFECIVE

AMBIENT TEMPERATURE °F. 45 OPERATORS AWG, DS, CSP



TEST TRAVERSES

TRAVERSE POINT	TIME (MIN.)	STACK GAS TEMP. (°F.)	S-TYPE PITOT ΔP (IN. H ₂ O)	VEL. (FT./ SEC.)	ORIFICE ΔP (IN. H ₂ O)	GAS METER VOLUME (FT. ³)	PROBE TEMP. (°F.)	OVEN TEMP. (°F.)	IMPINGERS TEMPERATURE (°F.)		GAS METER TEMP. (°F.)	PUMP VAC. (IN. Hg.)
									OUTLET	INLET		
	0	70				2230.46	230	230	46	135	53	
FM-1	5	90	0.26	21.39	0.81	2235.02	235	235	45	145	55	10.0
2	10	90	0.26	21.39	0.78	2239.50	240	240	48	185	57	10.0
3	15	95	0.18	19.77	0.76	2243.89	245	245	50	190	58	10.0
4	20	95	0.18	19.77	1.755	2248.29	240	252	55	200	60	10.0
5	25	100	0.20	20.93	1.755	2252.66	240	252	55	200	60	10.0
6	30	100	0.20	20.93	0.75	2257.05	240	251	55	200	60	10.0
TOTAL		AVERAGE		AV.		TOTAL			AVERAGE		AV.	

PARTICULATE SAMPLING DATA

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MOE
STANDARDS DEVELOPMENT BRANCH
LIBRARY